

PATENT COOPERATION TREATY

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NOTIFICATION OF ELECTION

(PCT Rule 61.2)

From the INTERNATIONAL BUREAU

To:

Commissioner
 US Department of Commerce
 United States Patent and Trademark
 Office, PCT
 2011 South Clark Place Room
 CP2/5C24
 Arlington, VA 22202
 ETATS-UNIS D'AMERIQUE
 in its capacity as elected Office

Date of mailing (day/month/year) 09 November 2000 (09.11.00)	
International application No. PCT/FI00/00249	Applicant's or agent's file reference 31805
International filing date (day/month/year) 24 March 2000 (24.03.00)	Priority date (day/month/year) 25 March 1999 (25.03.99)
Applicant PENTTILÄ, Merja et al	

1. The designated Office is hereby notified of its election made:

☒ in the demand filed with the International Preliminary Examining Authority on:
 18 October 2000 (18.10.00)

☐ in a notice effecting later election filed with the International Bureau on:

2. The election ☒ was
☐ was not

made before the expiration of 19 months from the priority date or, where Rule 32 applies, within the time limit under Rule 32.2(b).

The International Bureau of WIPO 34, chemin des Colombettes 1211 Geneva 20, Switzerland	Authorized officer F. Baechler
Fecsimile No.: (41-22) 740.14.35	Telephone No.: (41-22) 338.83.38

PATENT COOPERATION TREATY

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INTERNATIONAL SEARCH REPORT

(PCT Article 18 and Rules 43 and 44)

Applicant's or agent's file reference 31805	FOR FURTHER ACTION see Notification of Transmittal of International Search Report (Form PCT/ISA/220) as well as, where applicable, item 5 below.	
International application No. PCT/FI 00/00249	International filing date (day/month/year) 24 March 2000	(Earliest) Priority Date (day/month/year) 25 March 1999
Applicant Valtion teknillinen tutkimuskeskus et al		

This international search report has been prepared by this International Searching Authority and is transmitted to the applicant according to Article 18. A copy is being transmitted to the International Bureau.

This international search report consists of a total of 4 sheets.

☒ It is also accompanied by a copy of each prior art document cited in this report.

1. ☐ Certain claims were found unsearchable (See Box I).
2. ☐ Unity of invention is lacking (See Box II).
3. ☒ The international application contains disclosure of a nucleotide and/or amino acid sequence listing and the international search was carried out on the basis of the sequence listing
 - ☒ filed with the international application.
 - ☐ furnished by the applicant separately from the international application,
 - ☐ but not accompanied by a statement to the effect that it did not include matter going beyond the disclosure in the international application as filed.
 - ☐ transcribed by this Authority.
4. With regard to the title, ☐ the text is approved as submitted by the applicant.
☒ the text has been established by this Authority to read as follows:
 Process for partitioning of proteins.
5. With regard to the abstract,
 - ☐ the text is approved as submitted by the applicant.
 - ☒ the text has been established, according to Rule 38.2(b), by this Authority as it appears in Box III. The applicant may, within one month from the date of mailing of this international search report, submit comments to this Authority.
6. The figure of the drawings to be published with the abstract is:
 - Figure No. ☐ as suggested by the applicant. ☒ None of the figures.
 - ☐ because the applicant failed to suggest a figure.
 - ☐ because this figure better characterizes the invention.

Box III TEXT OF THE ABSTRACT (Continuation of item 5 of the first sheet)

The present invention relates to isolation and purification of proteins in aqueous two-phase systems (ATPS). Specifically the invention provides processes for partitioning of proteins of interest in ATPS by fusing said proteins targeting proteins which have the ability of carrying said protein into one of the phases.

A. CLASSIFICATION OF SUBJECT MATTER

IPC7: C07K 1/14, C07K 19/00, C12N 15/62, C12N 1/15 // C12R 1:885

According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC7: C07K

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

SE,DK,FI,NO classes as above

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
P,X	Journal of Chromatography A, Volume 839, 1999, Mårten Svensson et al, "Aqueous two-phase systems containing self-associating block copolymers. Partitioning of hydrophilic and hydrophobic biomolecules", page 71 - page 83, see abstract --	1,5-9,20-24
X	Journal of Chromatography A, 1996, Mats Carlsson et al: "Effects of fused tryptophan rich peptides to a recombinant protein A domain on the partitioning in polyethylene glycol-dextran and Ucon-dextran aqueous two-phase systems", page 107 - page 117, see abstract and sections 1 and 2 --	1,5-9,20-24

☒ Further documents are listed in the continuation of Box C.☒ See patent family annex.

* Special categories of cited documents:

- "A" document defining the general state of the art which is not considered to be of particular relevance
- "E" earlier document but published on or after the international filing date
- "L" document which may throw doubts on priority claim(s) or which is cited to establish the publication date of another citation or other special reason (as specified)
- "O" document referring to an oral disclosure, use, exhibition or other means
- "P" document published prior to the international filing date but later than the priority date claimed

"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention

"X" document of particular relevance: the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone

"Y" document of particular relevance: the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art

"&" document member of the same patent family

Date of the actual completion of the international search

14 July 2000

Date of mailing of the international search report

20 -07- 2000

Name and mailing address of the ISA/
Swedish Patent Office
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INTERNATIONAL SEARCH REPORT

International application No.

PCT/FI 00/00249

C (Continuation). DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	WO 9207868 A1 (KABI PHARMACIA AB), 14 May 1992 (14.05.92), see description, example 1 and claim 1 --	1,5-9,20-24
X	WO 9418330 A1 (UNILEVER PLC), 18 August 1994 (18.08.94) --	1,5-9,20-24
A	WO 9404673 A1 (OY ALKO AB), 3 March 1994 (03.03.94) --	16-18
A	Eur J Biochem, Volume 248, No 2, Sept 1997, Nakari-Setälä T et al, "Differential expression of the vegetative and spore-bound hydrophobins of Trichoderma reesei--cloning and characterization of the hfb2 gene", page 415 - page 423, see abstract --	16-18
A	Eur J Biochem, Volume 235, No 1-2, January 1996, Nakari-Setälä T et al, "Genetic and biochemical characterization of the Trichoderma reesei hydrophobin HFBI", page 248 - page 255, see abstract -- -----	16-18

INTERNATIONAL SEARCH REPORT

Information on patent family members

International application No.

02/12/95

PCT/FI 00/00249

Patent document cited in search report			Publication date	Patent family member(s)			Publication date
WO	9207868	A1	14/05/92	SE	9003534	D	00/00/00

WO	9418330	A1	18/08/94	AU	6139794	A	29/08/94
				EP	0682710	A	22/11/95
				FI	953792	A	10/08/95
				ZA	9400916	A	10/08/95

WO	9404673	A1	03/03/94	AU	4712193	A	15/03/94
				CA	2142602	A	03/03/94
				EP	0656943	A	14/06/95
				FI	950779	A	13/04/95
				JP	8500733	T	30/01/96

HAKEMUSNUMERO <i>Appl. no.</i> 990667	LUOKITUS C07K 1/14, 14/37, 19/00, C12N 15/63
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TUTKITTU AINEISTO
Patenttivirastojen julkaisut FI, SE, NO, DK, DE, CH, EP, WO, GB, US:
C07K 1, 3, 14, 19
C12N 15
Muu aineisto
EPO Documentation, EPO (EP, WO, CH, DE, FR, GB, US), European patent office
World Patents Index, Derwent
Chemical Abstracts, American Chemical Society

VIITEJULKAISUT		
Kategoria*)	Julkaisun tunnistetiedot	Koskee vaatimuksia
X	Journal of Chromatography A vol 839 (1999) ss. 71-83	23
X	J. Chem. Technol. Biotechnol. Vol 73 (1998) ss. 251-258	23
X	Colloids and Surfaces B: Biointerfaces vol 9 (1997) s. 109-116	23
X	Enzyme and Microbial Technology vol 19 (1996) ss. 507-517	23
X	Biotechnology and Bioengineering vol 49 (1996) ss. 290-299	23
X	Journal of Chemical Engineering of Japan vol 28 no 1 (1995) ss. 97-102	23
X	Solvent Extractions Res. Dev. JPN no 1 (1994) ss. 42-52	23
*) X Patentoitavuuden kannalta merkittävä julkaisu yksinään tarkasteltuna Y Patentoitavuuden kannalta merkittävä julkaisu, kun otetaan huomioon tämä ja yksi tai useampi samaan kategoriaan kuuluva julkaisu A Yleistä tekniikan tasoa edustava julkaisu, ei kuitenkaan patentoitavuuden este		
Päiväys 9.2.2000	Tutkija Arja Leikas	

PATENT COOPERATION TREATY

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INTERNATIONAL PRELIMINARY EXAMINATION REPORT

(PCT Article 36 and Rule 70)

Applicant's or agent's file reference 31805	FOR FURTHER ACTION See Notification of Transmittal of International Preliminary Examination Report (Form PCT/IPEA/416)	
International application No. PCT/FI00/00249	International filing date (day/month/year) 24.03.2000	Priority date (day/month/year) 25.03.1999
International Patent Classification (IPC) or national classification and IPC C 07 K 1/14, C 07 K 19/00, C 12 N 15/62, C 12 N 1/15		
Applicant Valtion teknillinen tutkimuskeskus et al		

1.	This international preliminary examination report has been prepared by this International Preliminary Examining Authority and is transmitted to the applicant according to Article 36.
2.	This REPORT consists of a total of <u>4</u> sheets, including this cover sheet.
<input type="checkbox"/>	This report is also accompanied by ANNEXES, i.e., sheets of the description, claims and/or drawings which have been amended and are the basis for this report and/or sheets containing rectifications made before this Authority (see Rule 70.16 and Section 607 of the Administrative Instructions under the PCT).
	These annexes consist of a total of _____ sheets.
3.	This report contains indications relating to the following items:
I	<input checked="" type="checkbox"/> Basis of the report
II	<input type="checkbox"/> Priority
III	<input type="checkbox"/> Non-establishment of opinion with regard to novelty, inventive step and industrial applicability
IV	<input type="checkbox"/> Lack of unity of invention
V	<input checked="" type="checkbox"/> Reasoned statement under Article 35(2) with regard to novelty, inventive step or industrial applicability; citations and explanations supporting such statement
VI	<input type="checkbox"/> Certain documents cited
VII	<input type="checkbox"/> Certain defects in the international application
VIII	<input type="checkbox"/> Certain observations on the international application

Date of submission of the demand 18.10.2000	Date of completion of this report 01.08.2001
Name and mailing address of the IPEA/SE Patent- och registreringsverket Box 5055 S-102 40 STOCKHOLM Facsimile No. 08-667 72 88	Authorized officer Carolina Gómez Lagerlöf/BS Telephone No. 08-782 25 00

Form PCT/IPEA/409 (cover sheet) (January 1998)

INTERNATIONAL PRELIMINARY EXAMINATION REPORT

International application No.

PCT/FI00/00249

I. Basis of the report

1. With regard to the elements of the international application:*

- ☒ the international application as originally filed
- ☐ the description:
pages _____, as originally filed
pages _____, filed with the demand
pages _____, filed with the letter of _____
- ☐ the claims:
pages _____, as originally filed
pages _____, as amended (together with any statement) under article 19
pages _____, filed with the demand
pages _____, filed with the letter of _____
- ☐ the drawings:
pages _____, as originally filed
pages _____, filed with the demand
pages _____, filed with the letter of _____
- ☐ the sequence listing part of the description:
pages _____, as originally filed
pages _____, filed with the demand
pages _____, filed with the letter of _____

2. With regard to the language, all the elements marked above were available or furnished to this Authority in the language in which the international application was filed, unless otherwise indicated under this item.

These elements were available or furnished to this Authority in the following language _____ which is:

- ☐ the language of a translation furnished for the purposes of international search (under Rule 23.1(b)).
- ☐ the language of publication of the international application (under Rule 48.3(b)).
- ☐ the language of the translation furnished for the purposes of international preliminary examination (under Rules 55.2 and/or 55.3).

3. With regard to any nucleotide and/or amino acid sequence disclosed in the international application, the international preliminary examination was carried out on the basis of the sequence listing:

- ☐ contained in the international application in written form.
- ☐ filed together with the international application in computer readable form.
- ☐ furnished subsequently to this Authority in written form.
- ☐ furnished subsequently to this Authority in computer readable form.
- ☐ The statement that the subsequently furnished written sequence listing does not go beyond the disclosure in the international application as filed has been furnished.
- ☐ The statement that the information recorded in computer readable form is identical to the written sequence listing has been furnished.

4. ☐ The amendments have resulted in the cancellation of:

- ☐ the description, pages _____
- ☐ the claims, Nos. _____
- ☐ the drawings, sheet/fig _____

5. ☐ This report has been established as if (some of) the amendments had not been made, since they have been considered to go beyond the disclosure as filed, as indicated in the Supplemental Box (Rule 70.2 (c)).**

* Replacement sheets which have been furnished to the receiving Office in response to an invitation under Article 14 are referred to in this report as "originally filed" and are annexed to this report since they do not contain amendments (Rules 70.16 and 70.17).

** Any replacement sheet containing such amendments must be referred to under item I and annexed to this report.

INTERNATIONAL PRELIMINARY EXAMINATION REPORT

International application No.

PCT/FI00/00249

V. Reasoned statement under Article 35(2) with regard to novelty, inventive step or industrial applicability; citations and explanations supporting such statement**1. Statement**

Novelty (N)	Claims	<u>2-24</u>	YES
	Claims	<u>1</u>	NO
Inventive step (IS)	Claims	<u>2-24</u>	YES
	Claims	<u>1</u>	NO
Industrial applicability (IA)	Claims	<u>1-24</u>	YES
	Claims	<u></u>	NO

2. Citations and explanations (Rule 70.7)

The claims disclose a process for partitioning of proteins or cells in aqueous two-phase systems (ATPS) by combining a protein or cell of interest to a targeting protein having the ability to partitioning in ATPS and subject this fusion protein to an ATPS separation. The claims further disclose a fusion protein containing a hydrophobin or hydrophobin-like protein fused to a protein for separation by ATPS.

During the search the following document were found:

- A Journal of Chromatography A, 1996, 107-117
- B WO 9207868 A1
- C WO 9418330 A1
- D WO 9404673 A1
- E Eur J Biochem, 1997, Vol 247, No 2, 415-423
- F Eur J Biochem, 1996, Vol 235, No 1-2, 248-255

Document A shows a method where a target protein has been fused to proteins or peptides to enhance the protein selectivity in partition systems. The proteins are specially design hydrophobic tetrapeptides or octapeptides containing tryptophan.

Document B discloses a method to enhance the partition coefficient of recombinant protein by modifying the product peptide by introducing tryptophan entities into the polypeptide chain of the product. The fusion protein contains the amino acid sequence $[\text{Ala}(\text{Trp})_n\text{Prom}]_m$, where n is 2 and m is an integer from 1-15.

.../...

INTERNATIONAL PRELIMINARY EXAMINATION REPORT

International application No.

PCT/FI00/00249

Supplemental Box

(To be used when the space in any of the preceding boxes is not sufficient)

Continuation of: V

It is known to enhance the partitioning ability of cells and proteins by fusing a protein of interest to a targeting protein. The known proteins contain tryptophan residues. In the description of the present application p 6, lines 27-31 it is stated that the targeting proteins of the invention are/can be larger than in the known small peptide tags of 12 amino acids. It is also stated the claimed proteins not necessarily contain tryptophan residues, but that they may do so. The scope of claim 1 covers all amphipathic and hydrophobic proteins that can be fused to a protein of interest to improve the ability to partition in ATPS, irrespective of if the contain tryptophan residues or not. The proteins in document B are covered by claim 1 in the present application.

Document C discloses a method for immobilising a binding protein capable of binding to a specific compound by linking it to the outside of a host cell. This protein is useful in protein isolation processes.

Documents D-E provide recombinant DNA sequences encoding for hfb1 and hfb2 and their ability to fuse antibodies.

Documents C-E show the general state of the art.

Thus, claim 1 is not considered to fulfil the requirements of novelty and inventive step.

Claims 2-24 are considered to fulfil the requirements of novelty, inventive step and industrial applicability.



INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

(51) International Patent Classification ⁷ : C07K 1/14, 19/00, C12N 15/62, 1/15 // C12R 1:885		A1	(11) International Publication Number: WO 00/58342
			(43) International Publication Date: 5 October 2000 (05.10.00)
(21) International Application Number: PCT/FI00/00249		(81) Designated States: AE, AG, AL, AM, AT, AU, AZ, BA, BB, BG, BR, BY, CA, CH, CN, CR, CU, CZ, DE, DK, DM, DZ, EE, ES, FI, GB, GD, GE, GH, GM, HR, HU, ID, IL, IN, IS, JP, KE, KG, KP, KR, KZ, LC, LK, LR, LS, LT, LU, LV, MA, MD, MG, MK, MN, MW, MX, NO, NZ, PL, PT, RO, RU, SD, SE, SG, SI, SK, SL, TJ, TM, TR, TT, TZ, UA, UG, US, UZ, VN, YU, ZA, ZW, ARIPO patent (GH, GM, KE, LS, MW, SD, SL, SZ, TZ, UG, ZW), Eurasian patent (AM, AZ, BY, KG, KZ, MD, RU, TJ, TM), European patent (AT, BE, CH, CY, DE, DK, ES, FI, FR, GB, GR, IE, IT, LU, MC, NL, PT, SE), OAPI patent (BF, BJ, CF, CG, CI, CM, GA, GN, GW, ML, MR, NE, SN, TD, TG).	
(22) International Filing Date: 24 March 2000 (24.03.00)		Published <i>With international search report.</i>	
(30) Priority Data: 990667 25 March 1999 (25.03.99) FI 19991782 20 August 1999 (20.08.99) FI			
(71) Applicant (for all designated States except US): VALTION TEKNILLINEN TUTKIMUSKESKUS [FI/FI]; Vuorimiehentie 5, FIN-02150 Espoo (FI).			
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(74) Agent: OY JALO ANT-WUORINEN AB; Iso Roobertinkatu 4-6 A, FIN-00120 Helsinki (FI).			
(54) Title: PROCESS FOR PARTITIONING OF PROTEINS			
(57) Abstract			
<p>The present invention relates to isolation and purification of proteins in aqueous two-phase systems (ATPS). Specifically the invention provides processes for partitioning of proteins of interest in ATPS by fusing said proteins to targeting proteins which have the ability of carrying said protein into one of the phases.</p>			

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Codes used to identify States party to the PCT on the front pages of pamphlets publishing international applications under the PCT.

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PROCESS FOR PARTITIONING OF PROTEINS

Field of the invention

5 The present invention relates to isolation and purification of proteins in aqueous two-phase systems (ATPS). Specifically the invention provides processes for partitioning of molecules of interest in ATPS by fusing said molecules to targeting proteins which have the ability of carrying said molecule into one of the phases.

10 **Background of the invention**

Liquid-liquid extraction in an aqueous two-phase system (ATPS) can offer a powerful technique for isolation and purification of proteins. The separation of macromolecules and particles by means of liquid-liquid extraction is well known (Albertsson, 1986; Walter *et al.*,
15 1985; Kula, 1990). Mainly polyethylene glycol (PEG) - salt, PEG-dextran and PEG-starch systems have been in use. More recently detergents and detergents with reversed solubility were discovered as suitable methods for separation of macromolecules, and especially for the separation of proteins.

20 An advantage of aqueous two-phase systems (ATPS) is that they are especially suited for large scale processing of microbial proteins not only from culture supernatants but also from crude extracts containing cells and cell debris (Kula, 1979; Kula, 1985). Characteristic features of biological fluids as well as suspensions are rather small particle sizes, low density differences between fluid and suspended solids, high viscosities of the extracts and high
25 compressibility of the solids (Hustedt *et al.*, 1985; Bender and Koglin, 1986). These attributes decrease the performance of conventional methods for solid-liquid separation like centrifugation and filtration at the beginning of a protein recovery process. Using an aqueous two-phase system removal of solids can be integrated into a liquid-liquid separation step, clarification is thus combined with an initial purification (Kula, 1979; Kula, 1985).

30

After the extraction process phase separation can be accomplished by settling under gravity as well as by centrifugation (Kula, 1985). ATPS can be applied in various scales from very

small laboratory scale to large industrial scale thus suiting for various proteins, purposes and needs. With regard to industrial purposes commercially available centrifugal separators can be used to shorten separation time. Several authors have investigated the potential of centrifugal separators of various design for processing of large volumes of aqueous two phase systems (Kula, 1979; Kula *et al.*, 1981, Kula *et al.*, 1982; Kula, 1985). In these studies the authors have used polymer/polymer or polymer/salt systems and the results of these investigations demonstrate the feasibility of continuous separation of aqueous two-phase systems in centrifugal separators.

Extraction systems based on nonionic surfactants have been described as an alternative to standard polymer/polymer or polymer/salt systems. Phase forming surfactants are e.g. polyoxyethylene type nonionic detergents. The basis of this type of aqueous two-phase system is the temperature-dependent reversible hydration of the polar ethylene oxide head groups. The temperature at which the phase separation occurs is referred to as the cloud-point (cloud-point extraction). This kind of aqueous two-phase system is especially suited for the extraction of amphiphilic biomolecules. The potential of this type of two-phase system for separating membrane bound proteins from cytosolic and peripheral membrane proteins was first demonstrated by Bordier (1981). Heusch and Köpp (1988) have been able to demonstrate that lamellar structures formed in the miscibility gaps of polyglycol ether / water systems are responsible for the selective extraction of hydrophobic substances.

Recently, the successful application of a surfactant-based aqueous two-phase system for the extraction of a membrane bound protein (cholesterol oxidase) from the unclarified culture medium of the gram-positive microorganism *Nocardia rhodochrous* on a bench scale has been reported (Minuth *et al.*, 1995). By addition of only one chemical compound a product release through solubilization was possible in homogeneous phase and in a second step a clarification as well as an initial purification was achieved by an extraction process at elevated temperatures separating the detergent rich phase. A closed concept was further developed for the production of the membrane bound enzyme by surfactant-based extraction, organic solvent extraction and anion-exchange chromatography, which gave a product suitable for analytical applications (Minuth *et al.*, 1996).

In aqueous two phase systems the desired target e.g. a protein should partition selectively into one phase (preferentially the lighter phase) while the other substances should partition into the other phase (preferentially the heavier phase). In PEG/salt and PEG/dextran and similar systems there are several driving forces for a substance like charges, hydrophobic, hydrophilic forces or the dependence on conformation or ligand interaction (Albertsson, 1986). The forces leading to separation in detergent based aqueous two phase systems are suggested to be primarily hydrophobic (Terstappen *et al.*, 1993). Even if a lot of work has been carried out in the field of prediction in ATPS, none of the designed models provides a physical picture of the phase behaviour and prediction is hardly possible (Johansson *et al.*, 1998).

In ATPS the partitioning coefficient is defined as the concentration (activity in case of an enzyme) of the target in the top phase divided by the concentration (enzyme:activity) of the target protein in the bottom phase. Partitioning coefficients in ATPS systems are usually in the range from less than 1 up to less than 100 (Terstappen *et al.*, 1992; Terstappen *et al.*, 1993).

$$K = \frac{C_{i,T}}{C_{i,B}}$$

Yield: is defined as the amount of target in the top phase divided by the sum of the amount of target in top and bottom. This leads to the following equation

$$Y_T = \frac{1}{1 + \left[\frac{V_B}{V_T} \cdot \frac{1}{K} \right]}$$

If the desired substance is directed to the heavier phase (as it can be the case using Triton) the yield is defined by

$$Y_B = \frac{1}{1 + \left[\frac{V_T}{V_B} \cdot K \right]}$$

The volume ratio of the two coexisting phases are defined by the volumes of the lighter over the heavier phase, respectively.

$$R = \frac{V_T}{V_B}$$

5 An example of useful proteins facing problems in purification in a cost-effective way are the commonly used industrial enzymes used as biocatalysts, the glycosyl hydrolases, proteases and lipases produced by fungi and bacteria. These are used in e.g. laundry, textile, paper and pulp, food and feed industry. The fact that microbes produce many different enzymes during their growth and the fact that some of these may be undesired in certain applications leads
10 to a need to enrich the active component(s). This enrichment can be performed by choosing appropriate growth conditions, by genetic engineering and/or by down-stream processing (e.g. purification of the active component(s)).

Purification of proteins are generally performed by chromatography. Usually gel-
15 chromatographic methods are used based on ion-exchange, hydrophobic interaction, affinity chromatography and molecular sieving. Methods like electrophoresis and crystallisation can also be used. These methods are well known in the art and suitable for proteins of fairly high market value. In case of bulky enzyme production these methods, however, are too expensive in order to keep the final product on a compatible price level. Due to similar
20 properties of these enzymes several purification steps are usually needed to separate the proteins from each other. This often causes low final yields and therefore a high loss of product.

Many extracellular hydrolases produced by the filamentous fungus *Trichoderma* are
25 currently used in different industrial applications in large scale. These hydrolases are e.g. hemicellulases (such as xylanases and mannanases), cellulases (such as endoglucanases and cellobiohydrolases) and proteases. Purification of these is well known in the art (Bhikhabhai *et al.*, 1984; Pere *et al.*, 1995), but for large industrial applications the purification methods are too expensive. Alternative methods to enrich these hydrolases have been used, including
30 deletion of undesired genes by genetic engineering (Suominen *et al.*, 1992). However, even

after extensive genetic engineering some minor undesired activities may still be present in the final product.

ATPS have been studied in purification of cellulases of *T. reesei* and the purification of an
5 endoglucanase III showed some promising results, enriching the yield of the protein in the upper phase (U.S. Pat. 5,139,943). ATPS have also been studied in purification of lipases, endoxylanase and natamycin (EP 0 574 050 A1). No K and Y values are, however, mentioned.

10 As in other protein purification methods, similar properties of proteins produced by an organism impair also in ATPS, e.g. selective separation of one protein is not achieved optimally. To obtain selectivity in purification affinity chromatographic methods are used especially for analytic purposes and in purification of high-value products. These include immunoaffinity chromatography and various fusion protein strategies well described in the
15 art such as fusing the protein of interest to an other protein (e.g. glutathione-S-transferase), protein domain (e.g. protein A-ZZ domain) or small peptide (e.g. His-tag), which selectively bind to the solid carrier and thus the recovery of the fusion partner is obtained as well. The fusion protein can be suitable for the particular purpose as such or cleavage of the product from the added fusion partner may be desired. There are well-known methods in the art on
20 cleavage of fusion proteins from their partners by proteases, e.g. by factor X, thrombin or papain or by genetically introducing a protease cleavage site (e.g. Kex2 site) or autoproteolytic domains (e.g. Intein, New England Biolabs) or by chemical cleavage (e.g. CNBr).

ATPS offer advantages mainly with respect to technology compared with the solid state
25 based separation systems e.g. affinity column-based techniques. The scale-up of extractive enzymes is relatively simple utilising commercially available equipment and machinery common in the chemical industry. In addition, it can be used in a continuous process and it can be relatively cost extensive. It can be used as a single step for clarification, concentration and purification. ATPS can be used as a first capture-step, but for bulk products often no
30 further purification is needed.

To aid selective separation in two-phase systems, recent publications have described the fusion of small peptide tags of 12 amino acids to the protein to be purified. The most successful of these soluble peptides are containing tryptophans. So far they have mainly been applied for very small molecules like the staphylococcal protein A derivative ZZT0
5 (Berggren *et al.*, 1999; Hassinen *et al.*, 1994; Köhler *et al.*, 1991).

Use of ATPS has so far been limited to certain targets. Due to the advantages of ATPS in protein separation, purification and localisation, highly selective and powerful methods should be developed. This is especially important for large scale processes where ATPS in
10 general is very inexpensive as a first capture step or as the only step for purification, clarification and concentration. The system should be universal so that the technique would be strong enough to mediate separation of in principle any component to the desired phase irrespective of its size or biochemical properties.

15 **Description of the invention**

In this invention we describe selective separation and partitioning of molecules and particles fusing them with targeting proteins having the capability to carry the molecule or particle of interest to the desired phase in ATPS, and to keep it in this phase if wanted. This
20 invention is directed to make ATPS usable for every biotechnological product. By addition of the targeting protein to selective products, either by genetic tagging of proteins, by chemical binding, glueing or by use of any other technique, the product molecule can be turned more suitable for separation in ATPS. Using ATPS the product or certain component is therefore driven to one phase while the other components or by-products are directed to
25 the other phase(s).

We also describe that efficient separation in ATPS can be obtained using targeting proteins which are/can be larger than the described small soluble synthetic peptide tags of 12 amino acids or less. These targeting molecules can aid in separating of small molecules but even
30 large proteins and particles. Unlike the small peptide tags, it is not necessary that they contain tryptophan residues, although they may do so. They can be hydrophobic or moderately hydrophobic and/or amphipathic in nature, either in monomeric form or when

forming aggregates. Such proteins can be found in nature or they can be designed, or obtained through for instance methods known in art for mutant generation, gene shuffling or directed evolution. Suitable targeting molecules can be screened for instance by fusion the product of interest to a library of natural or mutant sequences, and screening the ability of the fusion molecules to separate in ATPS. Furthermore, any molecule capable of separating in ATPS is a suitable targeting molecule.

Several techniques exploiting purified protein for isolation of the corresponding gene may be used to find genes encoding suitable targeting molecules for ATPS. Suitable proteins or polypeptides may be purified on the basis of their properties. They can be obtained by applying the cells, cell extracts or culture media to ATPS and recovering the proteins or peptides separated into the phase containing the hydrophobic phase material. Suitable targeting molecules may also be recovered for example from the culture medium foam formed either during the cultivation of a microorganism or caused by bubbling gas through the medium. Proteins and peptides suitable as targeting molecules may further be recovered from aggregates caused by freezing of culture media. After the targeting molecules have been purified, the corresponding genes are isolated using techniques known to a person skilled in the art. Such techniques include for example screening of expression libraries using antibodies raised against purified polypeptide or peptide, and PCR cloning and screening of genomic and/or cDNA libraries with oligonucleotides designed on the basis of N-terminal or internal protein sequences.

Examples of molecules suited as targeting proteins in ATPS found in nature are hydrophobin-like small proteins. Hydrophobins are secreted proteins with interesting physico-chemical properties that have recently been discovered from filamentous fungi (Wessels, 1994; Wösten and Wessels, 1997; Kershaw and Talbot, 1998). They are usually small proteins, approximately 70 to 160 amino acids, containing eight cysteine residues in conserved pattern, and do usually not contain tryptophanes. However, also multimodular proteins with one or several hydrophobin domains and e.g. proline-rich or asparagine/glycine repeats, or hydrophobins containing less than eight cysteine residues have been characterized (Lora *et al.*, 1994; Lora *et al.*, 1995; Arntz and Tudzynski, 1997). Hydrophobins have been divided into two classes based on their hydropathy profiles (Wessels, 1994).

Today most protein data exists for the hydrophobins Sc3p of *Schizophyllum commune* (class I), and cerato-ulmin of *Ophiostoma ulmi* and cryparin of *Cryphonectria parasitica* (class II), although more than 30 gene sequences for hydrophobins have been published (Wösten and Wessels, 1997). HFB genes are often naturally highly expressed but due to special requirements in cultivation conditions and the biochemical properties of the proteins, purification of HFBs in large amounts have been difficult. For instance only relatively moderate production levels of a few mg per liter of Sc3 hydrophobin in static cultures are obtained (Han Wösten, personal communication). Published purification procedures include e.g. multi-step extraction from fungal cell walls using organic solvents and bubbling or freezing of culture filtrates (Wessels, 1994). No reports of successful production of hydrophobins are available; levels of cerato-ulmin were no higher than those obtained with other naturally occurring fungal isolates (Temple *et al.*, 1997).

Upon shaking hydrophobin-containing solutions, the protein monomers form rodlet-like aggregates. These structures are similar to the ones found on surfaces of aerial structures. The self-assembly of purified Sc3 hydrophobin into a 10 nm thick amphipathic layer on hydrophilic and hydrophobic surfaces has been demonstrated (Wösten *et al.*, 1994a; Wösten *et al.*, 1994b). This film is very strongly attached to the surface and not broken, for instance, by hot detergent. The hydrophobic side of the layer on hydrophilic surfaces shows properties similar to teflon (Wessels, 1994). The Sc3 assemblages, as well as those of cerato-ulmin and cryparin, also form on gas-liquid or gas-air interphases thus stabilizing air bubbles or oil droplets in water.

Surface activity of proteins is generally low but hydrophobins belong to surface-active molecules, their surfactant capacity being at least similar to traditional biosurfactants such as glycolipids, lipopeptides/lipoproteins, phospholipids, neutral lipids and fatty acids (Wösten and Wessels, 1997). In fact Sc3 hydrophobin is the most potent biosurfactant known. It lowers the water surface tension to 24 mJm² at a concentration of 50 µg/ml due to a conformational change during self-assembly of monomers into an amphipathic film (Wösten and Wessels, 1997).

Hydrophobin-like molecules vary in their properties. For instance, rodlet-forming capacity has not been assigned for all hydrophobins (such as some class II), or they might have a weaker tendency to form stable aggregates (Russo *et al.*, 1992; Carpenter *et al.*, 1992). Another group of fungal amphiphatic proteins are repellents (Wösten *et al.*, 1996 (Ustilago),
5 for review, see Kershaw and Talbot, 1998). Consequently, other type of proteins suited as targeting proteins for ATPS, may have only some of the features assigned to hydrophobins. Other suitable proteins are hydrophobic ones such as e.g. lipases, cholesterol oxidase, membrane proteins, small peptide drugs like nisin, aggregating cell wall proteins, lipopeptides or any parts of these or combinations of these, and other molecules like glycolipids,
10 phospholipids, neutral lipids, fatty acids in combination with proteins or peptides.

In this invention the targeting protein, such as a hydrophobin-like protein or parts of it, is bound to the product molecule or the component to be separated. First, phase forming materials and eventually possibly also additional salts are added to a watery solution
15 containing the fusion molecule or component, and optionally also the contaminating materials. The added agents are mixed to facilitate their solubilization. As soon as they are solubilized the two phases are formed either by gravity settling or centrifugation. In the separation the target protein drives the product to for instance the detergent-rich phase which could either be the top or the bottom phase. The method is not only useful for
20 purification of products of interest but also for keeping the product or the component of interest, such as a biocatalyst, in a particular phase which enables certain useful biotechnical reactions.

Several ATPS systems are suitable for performing this invention. These include PEG
25 containing systems, detergent based systems and novel thermoseparating polymers. Detergent based systems can be nonionic, zwitterionic, anionic or cationic. The system can be based on amphiphilic polymeric detergents, micelle forming polymers. Novel polymers can be based on polyethylene-polypropylene copolymers such as pluronic block copolymers, Brij, polyoxyethylene derivatives of partial ethers of fatty acids made by adding polyoxyet-
30 hylene chains to the nonesterified body and polyoxyethylene derivatives. The well known PEG/salt, PEG/dextran and PEG/starch (or derivatives such as Reppal, hydroxypropyl starch) systems where PEG and water are forming the top phase and dextran/starch/salt and

water are forming the bottom phase. As salts are used phosphate, citrate, sulfate or others. In the present process the target is partitioning mainly to the top phase, while most of the contaminants are separating mainly to the bottom phase. Some hydrophobic contaminants might partition to the top phase as well. Using detergent based systems only one phase forming detergent has to be added. Optionally, salts and other chemicals can be used in addition. The mentioned chemicals are added, and the solution is mixed. After mixing the separation can take place either by centrifugation or gravity settling. In order to separate into two phases the temperature of the solution has to be over the cloud-point of the detergent. The solution has to be heated if the cloud-point is not reached otherwise. If wanted, a second separation step can follow after a first extraction step and the product rich phase can be further purified. Also the remaining product in the product poor and by-product rich phase can be re-extracted. Very good K values can be obtained and the yields and concentration factors are high.

The process of the present invention can advantageously be used in laboratory scale but is especially suitable for large scale separations. It can successfully be used in the separation of proteins and components from large fermentations. Using genetic modifications, the method can be used to purify any protein of interest including extracellular enzymes and proteins such as cellulases and hemicellulases from mixtures containing large amounts of protein such as several grams per liter. Furthermore, this separation can be obtained from various culture media including industrial media containing particular materials such as cellulose and spent grain. The method can be used to purify the product from culture media of strains modified not to produce endogenous hydrophobins. The separation can be done directly from the fermentation broth which can additionally contain cells, even viscous filamentous fungi. High biomass levels are acceptable for the process as explained in example 9. An example is the extracellular endoglucanase I from the fungus *Trichoderma reesei* which can be tagged for instance with the class 2 HFBI and can for example be separated with the nonionic polyoxyethylene C12-C18EO5. In this example the detergent rich phase is the lighter phase and contains most of the tagged endoglucanase while most of the other cellulases, proteases and other enzymes remain in the heavier phase. The mycelium separates to the bottom phase, too. The separation can be achieved using

separation temperatures higher than 25°C. The temperature can be decreased if certain salts like NaCl or K₂SO₄ are added.

The invention describes separation of molecules produced in various different organisms such as bacteria, yeast and filamentous fungi. The invention is suitable for purification of product molecules from extra- or intracellular locations, including cell wall bound molecules. It provides examples how the fusion molecule can be secreted by these different organisms but also provide an example how the fusion can be produced intracellularly.

10 The invention further describes how fusion molecules consisting of several domains can be constructed and successfully expressed and produced. The invention describes fusions of the targeting molecule to a small protein (CBD), to a moderately sized protein (EGI) and to a huge highly glycosylated protein (FloI), and different domain variations of these. These molecules can be ready as such for biotechnical use. Alternatively, the product can be
15 cleaved from the targeting protein by any method known in the art such as with proteases e.g. thrombin, factor X, papain or by chemical cleavage. Furthermore, ATPS is a preferential means to be used to separate the product from the targeting protein after cleavage, or these can be separated with other methods known in the art.

20 A suprising feature is that the targeting protein can also be used to carry large particles to the desired phase in ATPS. This can be obtained if the particles already contain proteins suited for targeting such as spores/conidia do in case of fungi. The targeting protein can also be attached to the particles or compounds *in vitro*. If cells are separated, the targeting protein can alternatively be expressed in the recombinant cells in such a way that it is
25 exposed at the cell surface whereby it mediates the separation of the cells in ATPS. A teaching how this can be done is provided in example 22. Other types of molecules which direct the targeting molecule to the cell surface can be found e.g. in the literature including bacterial outer membrane proteins and lipoproteins (Ståhl and Uhlén, 1997), and yeast proteins α -agglutinin and flocculin (Schreuder *et al.*, 1996; Klis *et al.* (1994) WO 94/01567; Frenken (1994) WO 94/18330).
30

A further advantage of the system is that the invention combined with ATPS provides a means to separate the product or desired component not only from other unnecessary or unwanted proteins but also from harmful proteins such as proteases as described in example 6. Thus, the invention is particularly suited for production and purification of heterologous proteins, e.g. sensitive mammalian proteins usually produced in limited amounts in heterologous hosts. Such proteins are for instance antibodies or fragments thereof, interferon, interleukin, oxidative enzymes and any foreign protein which can otherwise be produced in a host. It is possible that separation of the product from e.g. culture medium can also be obtained on-line or semi-continuously, thus minimising the effect of proteases or other harmful components present in the culture. When produced intracellularly, the invention also provides means to separate the heterologous product, for instance the inclusion bodies it may form, from the cellular extracts.

This invention describes for the first time that fusion proteins containing hydrophobin-like molecules can be made and produced in significant amounts despite the very particular properties of hydrophobin-like molecules. Importantly, this invention also describes how recombinant strains producing increased amounts of hydrophobin-like proteins as such can be made. This provides means to produce the targeting protein for uses in which it is wanted that the targeting protein is bound to the product or particle *in vitro*, to enable further separation of such molecules or particles in ATPS.

Importantly, this invention also describes how hydrophobin-like molecules can be purified in ATPS very efficiently with high K-values. The molecules can be separated in the same way as the above mentioned fusions, for instance by PEG systems or by detergent-based systems. Separation can be done from the culture medium or from cells. This provides a significant improvement in making pure preparates containing hydrophobin-like molecules since due to their properties their purification is very complicated and results in losses with the previously reported techniques as described above.

Brief description of drawings

Fig. 1 shows the map of the plasmid pMQ103.

- Fig. 2** shows the map of the plasmid pMQ113.
- Fig. 3** shows the map of the plasmid pMQ104.
- 5 **Fig. 4** shows the map of the plasmid pMQ114.
- Fig. 5** shows the map of the plasmid pMQ105.
- Fig. 6** shows the map of the plasmid pMQ115.
- 10 **Fig. 7** shows the map of the plasmid pMQ121.
- Fig. 8** Coomassie-stained 10% SDS-PAGE of the partitioning of EGIcore-HFBI fusion protein in two-phase separation using 5 % of the detergent C12-C18EO5. Lane 1, Molecular weight marker; Lane 2, Purified CBHI (4 µg);
- 15 Lane 3, Purified EGI (4 µg); Lane 4, 1/10 diluted VTT-D-98691 cellulose-based culture filtrate; Lanes 5 and 6, 1/10 diluted bottom phase and detergent phase (top phase), respectively, after separation of VTT-D-98691 culture filtrate with 5% detergent; Lane 7, Non-diluted bottom phase; Lane 8, Non-
- 20 diluted VTT-D-98691 cellulose culture filtrate.
- Fig. 9** Western analysis of the partitioning of EGIcore-HFBI fusion protein in two-phase separation by using different concentrations of the detergent C12-C18EO5. Fusion proteins were detected with anti-HFBI antibodies. Lane 1,
- 25 Molecular weight marker; Lane 2, Purified EGI; Lane 3, VTT-D-98691 cellulose culture filtrate; Lanes 4 and 5, Detergent phase (top phase) and bottom phase, respectively, after separation of VTT-D-98691 culture filtrate with 5% detergent; Lane 6, Same as lane 3, except 2 % detergent was used;
- 30 Lane 7, Same as lane 4, except 2 % detergent was used; Lane 8, Purified EGI; Lane 9; Purified CBHI.

- Fig. 10** Coomassie-stained 10% SDS-PAGE showing further purification of EGIcore-HFBI fusion protein from the endogenous CBHI when the top phase was re-extracted with 2% detergent. Lane 1, Molecular weight marker; Lane 2, Purified CBHI (4 μ g); Lane 3, Purified EGI (4 μ g); Lane 4, Detergent phase (top phase) after first extraction; Lane 5, Detergent phase (top phase) after second extraction.
- Fig. 11** Coomassie-stained 10% SDS-PAGE analysis of the EGI-HFBI protein when treated with thrombin. Lane 1, Molecular weight marker; Lane 2, EGI-HFBI (1 mg/ml) treated 72 h with 3 U of thrombin at 24°C; Lane 3, Same as lane 2, except no thrombin was added; Lane 4, EGI-HFBI (1 mg/ml) treated 48 h with 9 U of thrombin at 36°C; Lane 5, Same as lane 4, except no thrombin was added; Lane 6, Same as lane 5, except no incubation at 36°C.
- Fig. 12** shows the map of the plasmid pTNS13.
- Fig. 13** Western analysis of the partitioning of dCBD-HFBI fusion protein in two-phase separation using 5 % of the detergent C12-C18EO5. Fusion protein was detected with anti-HFBI antibody. Lane 1, Four times concentrated culture filtrate; Lane 2, Four times concentrated bottom phase; Lane 3, Top phase.
- Fig. 14** shows the map of the plasmid pTNS15. A non-functional restriction site is indicated with an asterisk.
- Fig. 15** shows the map of the plasmid pTNS18.
- Fig. 16** shows the map of the plasmid pTNS23.
- Fig. 17** shows that separation to the detergent phase of cells expressing a hydrophobin on cell surface occurs: the top detergent phase of *S. cerevisiae* VTT-C-99315 is turbid, whereas the top detergent phase of the control strain H2155 is clear.

- Fig. 18** shows the map of the plasmid pTNS32.
- Fig. 19** shows the map of the plasmid pTH4.
- 5 **Fig. 20** shows the map of the plasmid pTNS30.
- Fig. 21** shows the map of the plasmid pTH1.
- Fig. 22** shows the map of the plasmid pTH2.
- 10 **Fig. 23** shows the map of the plasmid pKS2.
- Fig. 24** SDS gel showing the purification of HFBI-dCBD in a Berol 532 ATPS system.
- 15 **Fig. 25** Western analysis of the partitioning of HFBI-ENA5ScFv fusion protein in two-phase separation using 4% of the detergent C12-C18EO5. Lanes from left: (1) Molecular weight marker, (2) Top (enriched) phase of the strain VTT-D-00791, (3) Bottom (depleted) phase of the strain VTT-D-00791.
- 20 **Fig. 26** Western analysis of the partitioning of SC3 hydrophobin using SC3 specific antibodies. Lane 1, Bottom phase of the strain VTT-D-00792, Lane 2, Top phase of the strain VTT-D-00792.
- Fig. 27** HPLC analysis for monitoring of the partitioning of HFBI in 2% Berol 532.
- 25 **Fig. 28** HPLC analysis for monitoring of the partitioning of HFBII in 2% Berol 532.

The invention is further illustrated by the following Examples which describe construction of the fusion molecules of the invention, and partitioning of the molecules of interest using
30 the process according to the invention.

EXAMPLES

Example 1

Construction of vectors for expression of EGI and EGIcore HFBI fusion proteins
5 under the *cbh1* and *gpd1* promoters of *Trichoderma* and *gpdA* promoter of *Aspergillus*

For construction of an EGI-HFBI fusion protein, *hfb1* (SEQ ID 1) coding region (from Ser-23 to the STOP codon) and a peptide linker (Val Pro Arg Gly Ser Ser Ser Gly Thr Ala Pro Gly Gly) preceding it was amplified with PCR using pTNS9 as a template and as a 5' primer
10 **TCG GG CACT ACG TG C CAG TAT AGC AAC GAC TAC TAC TCG CAA TGC**
CTT GTT CCG CGT GGC TCT AGT TCT GGA ACC GCA (SEQ ID 2) and as a 3' primer
TCG TAC GGA TCC TCA AGC ACC GAC GGC GGT (SEQ ID 3). pTNS9 has been
described in detail in Example 19. The sequence in bold in the 5' primer encodes 16 C-terminal
residues of EGI. The sequence in italics is a thrombin cleavage site and the underlined
15 CACTACGTG is a *DraIII* site. The underlined GGATCC in the 3' primer is a *BamHI* site.
The 280 bp PCR fragment was purified from agarose gel and ligated to pGEM-T T/A vector
(Promega) resulting in pMQ102.

For construction of an EGIcore-HFBI fusion protein, the *hfb1* coding region (as above) was
20 amplified with PCR using pTNS9 as a template and as a 5' primer **ACT ACA CGG AG G**
AGC TC G ACG ACT TCG AGC AGC CCG AGC TGC ACG CAG AGC AAC GGC
AAC GGC (SEQ ID 4) and as a 3' primer SEQ ID 3. The sequence in bold in the 5' primer
encodes amino acids 410-425 in EGI and the underlined GAGCTC is a *SacI* site. The 260 bp
PCR fragment was purified from agarose gel and ligated to pPCRII T/A vector (Invitrogen)
25 resulting in pMQ111.

In the next step *Trichoderma* expression vectors for production of EGI-HFBI and EGIcore-
HFBI fusion proteins under the control of *cbh1* promoter and terminator sequences were
constructed. The expression vector used as a backbone in the constructs is pPLE3 (Nakari *et*
30 *al.* (1994) WO 94/04673) which contains a pUC18 backbone, and carries the *cbh1* promoter
(SEQ ID 5) inserted at the *EcoRI* site. The *cbh1* promoter is operably linked to the full length
egl1 cDNA (SEQ ID 6) coding sequence and to the *cbh1* transcriptional terminator (SEQ ID

- 7). The plasmid pMQ102 was digested with *Dra*III and *Bam*HI and the released 280 bp fragment containing *hfbI* and linker sequences was purified from agarose gel and ligated to pPLE3 digested with *Dra*III and *Bam*HI. The plasmid pMQ111 was digested with *Sac*I and *Bam*HI and the 260 bp fragment containing the *hfbI* sequence was ligated to pPLE3 digested with *Sac*I and *Bam*HI. The resulting plasmids pMQ103 (Figure 1) and pMQ113 (Figure 2) carry the coding sequences for full-length EGI linked to HFBI via a peptide linker and for EGICore linked to HFBI via its own linker region, respectively, under the control of *cbhI* promoter and terminator sequences.
- 10 *Trichoderma* expression vectors for production of EGI-HFBI and EGICore-HFBI fusion proteins under the control of *gpdI* promoter and terminator sequences of *Trichoderma* and *gpdA* promoter and *trpC* terminator sequences of *Aspergillus* were constructed as follows. A *Sac*II site was inserted inbetween the *Xba*I and *Pac*I sites of pMV4 using as an adapter annealed primers TAA CCG CGG T (SEQ ID 8) and CTA GAC CGC GGT TAA T (SEQ ID 9). The resulting plasmid is pMVQ. pMV4 contains a pNEB193 (New England Biolabs) backbone, and carries a 1.2 kb *Trichoderma gpdI* promoter (SEQ ID 10) and a 1.1 kb *gpdI* terminator (SEQ ID 11) inserted at *Sal*I-*Xba*I and *Bam*HI-*Asc*I sites, respectively. The expression cassettes for EGI-HFBI and EGICore-HFBI were released from pMQ103 and pMQ113 with *Sac*II and *Bam*HI, purified from agarose gel and ligated to pMVQ cut with *Sac*II and *Bam*HI. The resulting plasmids pMQ104 (Figure 3) and pMQ114 (Figure 4) carry the EGI-HFBI and EGICore-HFBI cassettes, respectively, under the control of *Trichoderma gpdI* transcriptional control sequences. Expression plasmids pMQ105 (Figure 5) and pMQ115 (Figure 6) containing EGI-HFBI and EGICore-HFBI cassettes, respectively, operably linked to the *gpdA* promoter and *trpC* terminator of *Aspergillus* were constructed.
- 25 EGI-HFBI and EGICore-HFBI cassettes were released from plasmids pMQ104 and pMQ114 with *Xba*I and *Bam*HI, blunted with T4 DNA polymerase and ligated to *Nco*I digested and T4 DNA polymerase treated pAN52-1 (SEQ ID 12). pAN52-1 contains a pUC18 backbone, and carries a 2.3 kb *gpdA* promoter and a 0.7 kb *trpC* terminator sequences of *A. nidulans*.

Example 2**Construction of vectors for over-production of HFBI on cellulase-inducing and -repressing media**

5 For over-expression of HFBI under *cbh1* promoter the protein coding region of *hfb1* was amplified with PCR using as a template pEA10 (Nakari-Setälä *et al.*, 1996). pEA10 carries a 5.8 kb genomic *Sall* fragment containing *hfb1* coding and flanking sequences. **GTC AA C**
CGC GG A CTG CGC ATC ATG AAG TTC TTC GCC ATC (SEQ ID 13) was used as
 a 5' primer in the PCR and as a 3' primer SEQ ID 3. The sequence in bold in the 5' primer is
 10 21 bp of *cbh1* promoter adjacent to translational start site of the corresponding gene and the underlined CCGCGG is a *KspI* site. The obtained fragment of 430 bp was digested with *KspI* and *BamHI* and ligated to pMQ103 digested with *KspI* and *BamHI*. The resulting plasmid pMQ121 (Figure 7) carries the coding sequence of *hfb1* operably linked to *cbh1* transcriptional control sequences. pEA10 plasmid is used for over-production of HFBI in
 15 cellulase-repressing conditions.

Example 3**Transformation of *Trichoderma* and purification of the EGI-HFBI and EGIcore-HFBI producing and HFBI over-producing clones**

20 *Trichoderma reesei* strains QM9414 (VTT-D-74075) and Rut-C30 (VTT-D-86271) were co-transformed essentially as described (Penttilä *et al.*, 1987) using 3-13 µg of the plasmids pMQ103, pMQ113, pMQ104, pMQ114, pMQ105, pMQ115, pMQ121 and pEA10 and as the selection plasmids 1-3 µg pToC202, p3SR2 or pARO21. pToC202 (pUC19 backbone)
 25 and p3SR2 (pBR322 backbone) plasmids carry 2.7 kb *XbaI* and 5 kb *EcoRI-Sall* genomic fragments of *A. nidulans*, respectively, containing the *amdS* gene (Hynes *et al.*, 1983; Tilburn *et al.*, 1983). pARO21 is essentially the same as pRLMex30 (Mach *et al.* 1994) and carries the *E. coli hph* gene operably linked to 730 bp of *pki1* promoter and 1 kb of *cbh2* terminator sequences of *T. reesei*. The Amd⁺ and Hyg⁺ transformants obtained were streaked three
 30 times onto plates containing acetamide and hygromycin, respectively (Penttilä *et al.*, 1987). Thereafter spore suspensions were made from transformants grown on Potato Dextrose agar (Difco).

The production of the fusion proteins EGI-HFBI and EGICore-HFBI and HFBI was tested by slot blotting or Western analysis with EGI and HFBI specific antibodies from shake flask or microtiter plate cultivations carried out in minimal medium supplemented with either glucose, lactose or a mixture of Solka flock cellulose and/or spent grain and/or whey. The spore suspensions of the fusion protein producing clones were purified to single spore cultures on selection plates (containing either acetamide or hygromycin). To determine the best producers, production of the fusion proteins was analyzed again from these purified clones as described above.

T. reesei strains selected for further fermentor cultivations are VTT-D-98692 (pEA10), VTT-D-98492 (pMQ121), VTT-D-98693 (pMQ103), VTT-D-98691 (pMQ113), VTT-D-98681 (pMQ105) and VTT-D-98682 (pMQ115). These strains have QM9414 as the host strain. VTT-D-99702 (pMQ113) has Rut-C30 as the host strain.

Example 4

Cultivation of the EGI-HFBI and EGICore-HFBI protein producing and HFBI over-producing *Trichoderma* strains

EGI-HFBI and EGICore-HFBI fusions were produced under the *cbh1* promoter in a 15-litre fermenter using *T. reesei* strains VTT-D-98693 (pMQ103) and VTT-D-98691 (pMQ113), respectively. Strains were grown 5 days on minimal medium (Penttilä *et al.*, 1987) containing 4% Solka flock cellulose (James River Corporation, Berlin, NH) and 2 % spent grain (Primalco, Koskenkorva, Finland). EGICore-HFBI was also produced in fermenter (15 l) using the Rut-C30 strain VTT-D-99702 (pMQ113) with 4 % lactose medium. To induce the production of EGI-HFBI and EGICore-HFBI fusions under *Aspergillus gpdA* promoter, *T. reesei* strains VTT-D-98681 (pMQ105) and VTT-D-98682 (pMQ115) were cultivated in 15-litre fermenter. Strains were grown 3 to 5 days on minimal medium supplemented with 2% glucose, 0.2% Peptone, and 0.1% Yeast Extract, and with glucose feed to maintain the glucose concentration in the range of 1 to 3% throughout the cultivation. HFBI over-producing strain VTT-D-98692 (pEA10) was grown similarly in 15 l on glucose medium and the strain VTT-D-98492 (pMQ121) over-producing HFBI under *cbh1* promoter was

cultivated for 7 days in 15-litre fermentor on medium containing 4% Solka flock and 2% spent grain. The control cultivations with the host strains of the transformants, QM9414 (VTT-D-74075) and Rut-C30 (VTT-D-86271), were carried out on media containing i) Solka flock cellulose and either spent grain or whey, ii) lactose and iii) glucose similarly as described above.

When proper some *T. reesei* transformant strains and their host strains were also cultivated at 28°C in shake flasks for 5 to 6 days in 50 to 150 ml volume of *Trichoderma* minimal medium (Penttilä *et al.*, 1987) supplemented with either 3% Solka flock cellulose and 1% spent grain or 3-4% glucose with glucose feeding.

Example 5

Standard separation assays and analysis

If not otherwise stated the standard ATPS and subsequent analyses and calculations were carried out as explained in this example.

In general whole fermentation broth, supernatant (biomass separated by centrifugation or filtration) or purified proteins in buffer were separated in 10 ml graduated tubes. First detergent was added into the tubes and the tubes were then filled to 10 mg with protein containing liquid. The amount of detergent in the tube was calculated in weight percent of detergents. After thorough mixing in an overhead shaker the separation took place by either gravity settling in a water bath at constant temperature or by centrifugation at constant temperature. The separation usually was performed at 30°C, the standard amount of detergent used was 2-5% (w/v). After separation the volume ratio was noted and samples were taken from the lighter and heavier phase for analysis.

Two-phase separations were analysed qualitatively by using SDS-PAGE gels followed by visualization of the fusion proteins with Coomassie brilliant blue R-250 (Sigma) or Western blotting. Polyclonal anti-HFBI antibody were used in Western analysis for detection of EGIcore-HFBI, EGI-HFBI and dCBD-HFBI proteins together with alkaline phosphatase conjugated anti-rabbit IgG (Bio-Rad). Alkaline phosphatase activity was detected

colorimetrically with BCIP (5-bromo-4-chloro-3-indolyl-phosphate) used in conjunction with NBT (nitro blue tetrazolium) (Promega).

Contaminating endogenous EGI, CBHI and EGIII in the top phase was tested with appropriate antibodies. Acidic protease activity in the top and bottom phase was also tested using the SAP method (Food Chemicals Codex, p. 496-497, 1981), which is based on the 30 min enzymatic hydrolysis of a hemoglobin substrate. All reactions were performed at pH 4.7 and 40 °C. Unhydrolyzed substrate was precipitated with 14% TCA and removed by filtration. The released tyrosine and tryptophan was determined spectrophotometrically. Total protein concentrations were determined by *Non-Interfering* Protein AssayTM (Geno Technology, Inc).

EGI activity was detected using 4-methylumbelliferyl-β-D-cellobioside (MUC) (Sigma M 6018) as substrate (Van Tilbeurgh H. & Caeyssens M., 1985; Van Tilbeurgh *et.al.*, 1982). EGI hydrolyses the β-glycosidic bond and fluorogenic 4-methylumbelliferone is released, which can be measured using a fluorometer equipped with a 360 excitation filter and a 455 nm emission filter. CBHI also hydrolyses the substrate and it was inhibited by addition of cellobiose (C-7252, Sigma). EGI containing liquid was added in an appropriate dilution to a buffer containing 50 mM sodium acetate buffer (pH 5), 0.6 mM MUC and 4.6 mM cellobiose. The mixture was heated to 50°C. The reaction was stopped after ten minutes using 2% Na₂CO₃, pH 10. Purified CBHI was detected using the same assay as for EGI without the addition of the inhibitor cellobiose.

The partition coefficient K was defined as the ratio of the measured concentrations or activities in the top and bottom phase, respectively.

The Yield Y was defined as follows:

$$Y_T = \frac{1}{1 + \left[\frac{V_B}{V_T} \cdot \frac{1}{K} \right]}$$

where Y_T is the Yield of the top phase, V_B and V_T are the volumes of top and bottom phase, respectively. The Yield of the bottom phase can be described accordingly.

The mass balances, e.g. recovery of all added protein, were always checked for completeness to ensure no artificially high Yield (e.g. due to possible inactivation of the protein in the bottom phase). The values were usually calculated based on total enzyme activity (EGI wt plus the EGI-fusion) and thus the values are underestimated for the separation of the fusion as demonstrated in Example 16.

Example 6

Small scale ATPS separation studies and gel analysis

EGI-HFBI and EGICore-HFBI fusions produced under the *cbhI* promoter in a 15-litre fermenter on Solka flock cellulose and spent grain medium as described in Example 4 using *T. reesei* strains VTT-D-98693 (pMQ103) and VTT-D-98691 (pMQ113), respectively, were separated in small scale ATPS as described above.

The phases from the two phase separations were analysed qualitatively by using SDS-PAGE gels followed by visualization of the fusion proteins with Coomassie brilliant blue or Western blotting. Coomassie stained SDS-PAGE (10%) is shown in Figure 8. In the lane containing the non-extracted culture filtrate three distinct closely migrating bands can be seen (the sample was diluted 1/10 with H₂O). The topmost band is CBHI, the band in the middle is EGICore-HFBI fusion and the lower one endogenous EGI. In the samples separated in ATPS, only two bands (CBHI and EGI) are seen in the sample from bottom phase and one band representing EGICore-HFBI in the sample obtained from the top phase.

Western blotting with HFBI antibody showed thick bands for the top phase, whereas for the bottom phase there was only faint band demonstrating that the fusion is separating strongly into the detergent top phase. Figure 9 shows the separation of the EGICore-HFBI fusion produced on cellulose media into the top phase. Contaminating endogenous EGI and EGIII in the top phase was tested with appropriate antibodies but no signal was detected.

Small amount of endogenous CBHI was found in the upper phase when CBHI antibody was used in Western blotting. EGI, EGIII and proteases were not found in the top phase. Further purification from the contaminating CBHI was observed when the top phase was re-extracted

with 2 % detergent. The Figure 10 shows that the upper phase does not any more contain CBHI and pure fusion protein is recovered.

EGIcore-HFBI was also produced in fermenter (15 l) using the Rut-C30 strain VTT-D-99702 (pMQ113) with 4 % lactose medium. The separation in ATPS carried out in the standard manner gave essentially the same result as the separation from cellulose containing medium thus demonstrating that the purification can be carried out from several media relevant for large scale industrial use.

- 10 Acidic protease activity in the top was only 1/15 compared to the bottom phase (table below) demonstrating that acidic proteases remain in the bottom phase.

	A (275 nm)	HUT ³ /ml
Bottom phase ¹	0.146	41.6
Top phase ²	0.009	2.6

¹1/10 diluted bottom phase after separation of VTT-D-98691 culture filtrate with 2% detergent

- 15 ²1/100 diluted bottom phase after separation of VTT-D-98691 culture filtrate with 2% detergent

³1 HUT = enzyme concentration, which in reaction conditions hydrolyses hemoglobin in 1 min so that the absorbance at 275 nm of the formed hydrolysate equals 1.10 µg tyrosine/ml 0.006 N HCl solution.

- 20 These results show that the fusion protein can be purified extremely efficiently and the resulting preparate is free of other proteins produced by the fungus including proteases.

Example 7

Recovery of the native EGI in ATPS after thrombin cleavage

- 25 EGI-HFBI protein produced by the strain VTT-D-98693 has a thrombin cleavage site (LVPRGS) designed in the linker region between the EGI CBD and HFBI, which would enable the recovery of the native EGI after thrombin cleavage. EGI-HFBI fusion protein was purified from the culture filtrate (100 ml) of strain VTT-D-98693 grown on 4% Solka flock

cellulose and 2 % spent grain as described in Example 4 using the 2-phase separation system (5 % detergent). After removal of the bottom phase the detergent phase was extracted by isobutanol. The resulting water phase (~19 ml) was divided in eppendorf tubes and the liquid was evaporated with speed vac. Remaining lyophilizate was diluted to 50 mM Tris-Cl (pH 8).

- 5 To test the efficiency of thrombin cleavage, 9 units of thrombin (Sigma) was incubated > 24 h with 1 mg EGI-HFBI fusion protein in 36 °C at pH 8.0. Coomassie stained SDS-PAGE (10 %) was used for detection.

Only minor cleavage was observed in 48 h under these conditions (Figure 11), possibly due to
10 steric hindrance by O-glycosylation in the linker.

Example 8

Separation of low concentrations of EGICore-HFBI in ATPS

- 15 Detergent based aqueous two-phase systems were successfully applied using very low concentrations (diluted) of EGICore-HFBI fusion protein produced with the *cbh1* promoter in *T. reesei* VTT-D-98691 (pMQ 113) from a 15 liter cultivation carried out on Solka flock cellulose with spent grain as described in Example 4.
- 20 The original protein concentration of the supernatant was 7.0 mg/ml. This supernatant was diluted with de-ionised water by a factor of 100 and 1000, respectively. The fusion protein could be separated using 2% (w/w) of the detergent C12-C18EO5 with partitioning coefficients higher than 5. This is shown in the table below together with the experiment with non-diluted supernatant. The partitioning coefficients were calculated based on activity
25 measurements for total EGI (wild type and fusion protein together).

	EGICore-HFBI non-diluted supernatant	dilution 1/100	dilution 1/1000
K	4.1	5.3	5.6
Y [%]	38	31	32

Example 9**Separation of EGlcCore-HFBI from fungal biomass containing culture broths**

- EGlcCore-HFBI from *T.reesei* strain VTT-D-98691 (pMQ 113-2) was cultivated (50 ml in 250 ml shake flasks) on Solka flock cellulose with spent grain as described in Example 4. Directly after the cultivation, part of the whole broth was centrifuged at 3000 rpm for 30 min, supernatant was spilled out and the centrifuged mycelium was added to the supernatant to obtain artificial whole broths containing different amounts of biomass.
- Using 5% of C12-C18EO5 in a 10 g experiment consisting of up to 50% wet biomass (weight of wet biomass divided by the sum of wet biomass and supernatant) could still be separated without any difficulties. The Yield remained in between 61 and 64 % and therefore it is not significantly different in comparison to the experiment carried out with supernatant only (without mycelium) (see table below). The total recovery of the fusion protein is even higher. This is most probably due to cell attached enzyme extracted in the ATPS increasing the total amount of EGI. The partitioning coefficient was calculated based on activity measurements for total EGI (wild type and fusion protein together).

	K	Y[%]
Supernatant	5.5	62
25% of wet biomass in supernatant	7.3	66
40% of wet biomass in supernatant	6.4	61
50% of wet biomass in supernatant	7.6	64

Example 10**Separation of EGI-HFBI in ATPS**

EGI-HFBI from *Trichoderma reesei* strain VTT-D-98693 (pMQ 103) from a 15 liter cultivation carried out on Solka flock cellulose and spent grain as described in Example 4 was separated in a 10 g experiment using different amounts of C12-C18EO5. The partitioning coefficients are shown below. The partitioning coefficient was calculated based on activity measurements for total EGI (wild type and fusion protein together), and as in previous examples the endogenous EGI is included in the partitioning coefficients.

Detergent [% w/w]	2	3	5	7
K	1.9	1.8	1.4	1.1

Example 11**Separation of EGICore-HFBI in 50 ml**

EGICore-HFBI from *T. reesei* strain VTT-D-98691 (pMQ 113) cultivated in 15 liters using Solka flock cellulose and spent grain as described in Example 4 was separated in Falcon tubes in a 50 g experiment using 5% of C12-C18EO5. A partition coefficient of 2.52 and a yield of 51 % could be obtained. The separation was performed at 30°C at 3000rpm for 30 minutes.

The values are based on activity measurements for total EGI activity (wild type and fusion protein together) including endogenous EGI.

Example 12**Separation of EGICore-HFBI in ATPS using different detergents**

EGICore-HFBI from *T. reesei* strain VTT-D-98691 (pMQ 113) cultivated in 15 liters using Solka flock cellulose with spent grain as described in Example 4 was separated in a 10 g experiment using 2% of detergent in each experiment. The detergents investigated in this example were C10 EO5, C12 EO5, C14 EO6 (each Nikko Chemicals, Japan), C12-C18 EO5

(„Agrimul NRE 1205“, Henkel, Germany), C12/14 5EO, C12/14 6EO (Clariant, Germany), C9/11 EO5.5 („Berrol 266“, Akzo Nobel, Germany), Triton X-114 (Sigma, Germany). The partition coefficients and yields are listed below. The values are based on activity measurements for total EGI activity (wild type and fusion protein together) including
 5 endogenous EGI.

	K	Y(fusion) [%]
C10EO5	20	56
C12EO5	15	57
C12-C18EO5	14	66
C12/14 5EO	12	58
C12/14 6EO	14	62
C14EO6	11	54
C9/11 EO5.5	5	30
Triton X-114	0.16	53

10 Example 13

Separation of EGIcore-HFBI in ATPS from glucose grown cultures

EGIcore-HFBI was separated from cultivation of the *Trichoderma reesei* strain VTT-D-98682 (pMQ115) cultivated with glucose as described in Example 4. The supernatant was
 15 separated with 2% of the detergent C12-C18 EO5. The fusion protein could be partitioned with a K value of 2.4. In comparison, the K value for the native EGI is 0.3 when measured in a similar way for purified EGI.

Example 14

20 Separation of EGIcore-HFBI using different concentrations of detergent

EGIcore-HFBI from *T. reesei* VTT-D-98691 (pMQ 113) cultivated in 15 litres using Solka flock with spent grain as described in Example 4 was separated in detergent based ATPS

applying different amounts of the detergent C12-C18 EO5 on the cell free supernatant. The partitioning coefficients are shown in the table below. The corresponding gel electrophoresis and Western antibody-blot are shown in Figure 8 and Figure 9, respectively.

The values are based on activity measurements of total EGI activity.

5

Amount of detergent C12-C18 EO5	K	Yield(%)
1.0%	6.1	9
2.0%	4.1	38
3.5%	3.6	50
5.0%	2.9	55
7.5%	1.7	53
10.0%	1.1	58

Example 15

Re-extraction of the detergent phase

10

Detergent based ATPS was applied on EGIcore-HFBI fusion protein containing supernatant produced by the strain VTT-D-98691 (pMQ 113) in a shake flask cultivation. The first extraction using C12-C18EO5 conducted under the standard conditions shows a partitioning coefficient of 16 and a yield of 72 % (wild type EGI measured together with fusion protein).

15 The top phase was re-extracted in 10 mM sodium acetate buffer (pH 5) with 2% of detergent. A partitioning coefficient of 52 and a yield of 89 % could be obtained. In the re-extraction experiment of the bottom phase (2% of detergent), a small yield of 7.5% and a K of 0.8 of EGI activity were achieved. The partitioning coefficients were calculated based on activity measurements for total EGI (wild type and fusion protein together). Due to the wild

20 type EGI present in the sample, the yield is at least 72% and the partitioning coefficient at least 16 in the first extraction. The SDS-PAGE results of both extractions are shown in Figure 10.

Separation step	K	Y[%]
2% detergent	16	72
reextraction top phase	52	89
reextraction bottom phase	0.8	7.5

Example 16

Separation of pure cellulases in ATPS

5

The effect of HFBI on partitioning and the final yield can further be demonstrated by comparing the extraction result of EGIcore-HFB fusion with extraction results obtained with purified wild type EGI and EGIcore. The fusion protein is partitioning more than 100 times better to the detergent phase (see table below).

10

The improvement on the partitioning of the purified fusion protein from the first extraction obtained in the re-extraction (see Example 15) can be explained by the partitioning of the wild type EGI as demonstrated with purified wild type EGI in the table below. The wild type EGI lowers the partitioning coefficient in the first extraction (since EGI activity is measured from both top and bottom phase), but the absence of it in the re-extraction increases the partitioning coefficient of the EGIcore-HFBI fusion. The purity can in addition be demonstrated by analysing the partitioning of pure CBHI, which is the major contaminating protein corresponding to about 50 % of all secreted *T. reesei* proteins. Pure CBHI has a partitioning coefficient of 0.5 and a yield of 3.6 and is therefore separated from the fusion protein.

20

Separation step	K	Y[%]
re-extraction of top phase	52	89
extraction of pure wild type EGI	0.3	2.2
extraction of pure EGI-core	0.3	2.3
extraction of pure CBHI	0.5	3.6

Using the definitions of K and Y and calculating mass balances, the ratio of the amount of EGI fusion protein to EGI wild type can be calculated. The "true" partition coefficients and Yields can be concluded from this. "True" means the values which would be detected if it would be possible to measure only the amount of EGI-fusion without measuring the amount for EGI wild type at the same time.

The fundament for the calculation is the re-extraction experiment. The re-extracted top phase is believed to be pure. An example of the measured values and the calculated "true" values based on this are shown in the table below for two cultivations of VTT-D-98691 (pMQ113) grown as described in Example 4.

cultivation vessel	cultivation substrate	K "with EGI wt"	"true" K	Y [%] "with EGI wt"	"true" Y [%]
15 liter fermenter	whey permeate	4	6	16	54
250 ml shake flask	cellulose	16	54	66	90

Example 17

HFBI and HFBII purification in ATPS

HFBI was produced by cultivating the *T. reesei* strain VTT-D-98692 (pEA10-103B) using glucose as substrate as described in Example 4. HFBI could be separated using 2% of the detergent C12-C18 EO5 with a partition coefficient higher than 20 under the standard conditions described.

HFBII was produced by cultivating the *T. reesei* strain VTT-D-74075 (QM9414) on whey spent grain as described in Example 4. HFBII could be separated using 2% of the detergent C12-C18 EO5, exceeding a partition coefficient of 10 under the standard conditions.

Both HFBI and HFBII hydrophobins are thus partitioning well to the upper phase in ATPS.

Example 18**Detergent based ATPS with additional NaCl**

EGIcore-HFBI from which cultivation of *T. reesei* was separated in a 10 g experiment using
 5 5% of C12-C18EO5. The partitioning coefficient of the supernatant was 3.5 with a volume
 ratio of 0.2. Using 1.1 % (w/v) NaCl the partitioning coefficient could be increased to 4.3
 with a lower volume ratio of 0.14.

Example 19

10 **Construction of an *E. coli* strain expressing a fusion protein HFBI-dCBD, containing
 hydrophobin I and double cellulose binding (CBD) domains**

A 280 bp DNA fragment containing a modified *cbh2* linker region followed by the coding
 region of *hfb1* from Ser-23 to the STOP codon was amplified by PCR using the plasmid
 15 pARO1 (Nakari-Setälä *et al.*, 1996) as a template. The 5' primer was 5' TCT AGC AAG
CTT GGC TCT AGT TCT GGA ACC GCA CCA GGC GGC AGC AAC GGC AAC
 GGC AAT GTT TGC (SEQ ID 14) and the 3' primer was 5' TCG TAC AAG CTT TCA
 AGC ACC GAC GGC GGT (SEQ ID 15). The sequences in bold in the 5' and 3' primers
 encode the modified CBHII linker (Gly Ser Ser Ser Gly Thr Ala Pro Gly Gly) and a
 20 translational STOP, respectively, and the underlined AAGCTT in both primers is a HindIII
 site. The PCR fragment was purified from agarose gel, digested with HindIII and ligated to
 HindIII digested and SAP treated (Shrimp Alkaline Phosphatase, USB) pSP73 resulting in
 plasmid pTNS9.

25 For subsequent cloning of the modified CBHII linker-HFBI fragment to an *E. coli* expression
 vector, pTNS9 was digested with HindIII and the proper fragment was purified from agarose
 gel. This HindIII fragment was cloned to HindIII digested and SAP treated (Shrimp Alkaline
 Phosphatase, USB) B599 resulting in pTNS13 (Figure 12). The *E. coli* expression vector
 B599 is essentially the same as the one described by Linder *et al.* (1996) except that it is
 30 missing a STOP codon at the end of the protein coding sequence. It carries the coding
 sequence for a fusion protein containing CBHII CBD (41 N-terminal residues of CBHII) and
 CBHI CBD linked together via CBHI linker region (CBHI linker and CBD are the last 57

residues in CBHI). The expression and secretion of the fusion protein in B599 is under the control of *tac* promoter and *pelB* signal sequence (Takkinen *et al.*, (1991). pTNS13 expression vector thus carries the coding region for a fusion protein of double CBD and HFBI linked in frame via the Gly-Ser-Ser-Ser-Gly-Thr-Ala-Pro-Gly-Gly peptide. This vector also contains
5 the *amp* gene for selection of *E. coli* transformants. pTNS13 plasmid was transformed into *E. coli* strain RV308 (*su-*, Δ *lacX74*, *galISII::OP308*, *strA*) and this strain was used for production of the fusion protein.

Example 20

10 Separation of HFBI-dCBD molecules expressed in *E. coli* in ATPS

dCBD-HFBI was produced in *E. coli* strain RV 308 transformed with pTNS13 plasmid as described above. The inoculum of RV308/pTNS13 was grown to the exponential growth phase in LB medium containing ampicillin (0.1 g/l) and 1% glucose. Fermentation was carried
15 out using mineral salt medium described by Pack *et al.* (1993) with glucose (feed) in 10 litre fermenter. During cultivation temperature was maintained at 28 °C and pH was controlled at 6.8 with NH₄OH. Cell growth was monitored by measuring OD₆₀₀ and dry weight of biomass. The culture was induced with 50 µM (final concentration) IPTG (isopropyl-β-D-thiogalactopyranoside) at late-exponential growth phase (OD₆₀₀=50-60) to promote fusion
20 protein production.

Two-phase separation analysis of dCBD-HFBI protein was performed using culture filtrate and 5% detergent in the total volume of 40 ml. Results from Western blotting showed that 2-phase separation with 5 % detergent in the standard way was highly specific also for the
25 dCBD-HFBI fusion. Strong signal was observed in the sample from the detergent phase compared to the sample from the bottom phase as shown in Figure 13.

Example 21**Construction of yeast strains expressing HFBI-FloI fusion protein on the cell surface**

- For construction of a HFBI-FLO1 fusion protein expression cassette, *hfb1* (SEQ ID 1) coding region (from Ser-23 to the STOP codon) was amplified with PCR using pARO1 (Nakari-Setälä *et al.*, 1996) as a template and as a 5' primer TCT AGC TCT AGA AGC AAC GGC AAC GGC AAT GTT (SEQ ID 16) and as a 3' primer TGC TAG TCG ACC TGC TAG CAG CAC CGA CGG CGG TCT G (SEQ ID 17). The underlined sequences in the 5' and 3' primers are XbaI and NheI sites, respectively. The 0.225 bp PCR fragment was purified from agarose gel and ligated to pGEM-T vector (Promega) resulting in pTNS10. The *hfb1* fragment was released from pTNS10 with XbaI and NheI and ligated to pTNS15 cut with the same restriction enzymes. Plasmid pTNS15 (Figure 14) is essentially the same as plasmid pBR-ADHI-FLOIL by Watari *et al.* 1994 except that a NheI site in the pBR322 backbone has been replaced by a BglII site and a unique XbaI site is introduced by linker cloning in the unique AocI site preceding the putative signal sequence cleavage site. The resulting plasmid pTNS18 (Figure 15) contains the complete expression cassette for HFBI-FLO1 fusion protein in which HFBI substitutes the putative lectin domain from Ser-26 to Ser-319 in the yeast flocculin FLO1 (SEQ ID 18).
- In the next step, yeast expression vector for production of HFBI-FLO1 fusion protein was constructed. The expression vector used as a backbone in the construct is pYES2 (Invitrogen) (SEQ ID 19) which is a high-copy episomal vector designed for inducible expression of recombinant proteins in *S. cerevisiae*. It carries *GAL1* promoter and *CYC1* terminator sequences which regulate transcription, and 2 μ origin of replication and *URA3* gene for maintenance and selection in the host strain. The plasmid pTNS18 was digested with HindIII and the released 3.95 kb fragment containing the expression cassette for HFBI-FLO1 was purified from agarose gel and ligated to pYES2 digested with HindIII. This ligation mixture was concentrated by standard ethanol precipitation. The ligation mixture should contain besides unligated fragments and uncorrect ligation products also molecules where the vector and insert are correctly ligated with each other to result in plasmid pTNS23 (Fig. 16) which carries the expression cassette for HFBI-FLO1 operably linked to *GAL1* and *CYC1* terminator sequences.

The above ligation mixture was transformed using the LiAc method of Gietz *et al.* (1992) into a laboratory *S. cerevisiae* strain H452 (wild type W303-1A; Thomas and Rothstein, 1989). Transformant colonies able to grow on SC-URA plates were picked and streaked on selective plates. Nitrocellulose replicas were taken from the plates and treated for colony hybridization according to Sherman *et al.* (1983). To find those yeast colonies containing the pTNS23 plasmid, replicas were hybridized with digoxigenin labelled *hfb1* coding fragment after which an immunological detection was performed all according to the manufacturer (Boehringer Mannheim). Plasmids were recovered from several yeast colonies giving positive hybridization signal by isolating total DNA and using this in electroporation of *E. coli*. Restriction mapping and sequencing were carried out to confirm that the pTNS23 plasmid in the yeast transformants was correct. One of the transformants carrying plasmid pTNS23 was chosen for further studies and was designated VTT-C-99315. The control strain for it is yeast strain H2155 which carries the plasmid pYES2 in H452 background.

Example 22

Separation of yeast cells expressing HFBI-Flo1 fusion protein in ATPS

The *Saccharomyces cerevisiae* strain VTT-C-99315 (vector pTNS23) and its control strain H2155 (vector pYES2) were cultivated on synthetic complete medium lacking uracil (SC-URA) (Sherman, 1991) with 2% galactose as the carbon source to give an A_{600} of approximately 4. Approximately 6.3×10^8 cells in their culture medium were taken to ATPS using 7% (w/v) C12-18EO5 detergent (Agrimul NRE from Henkel) in a total volume of 5 ml. ATPS was carried out using standard protocol. After phase separation by gravity settling, the top detergent phase was clearly turbid in the case of the strain VTT-C-99315 in contrast to the control strain whose detergent phase was clear (Figure 17). Samples were taken from the top phases and dilution series from 10^{-1} to 10^{-5} were prepared in 0.9% NaCl and plated on YPD plates. After incubation at 30°C the amount of yeast colonies were calculated showing at least 70 times more yeast colonies of the strain VTT-C-99315 on YPD plates compared to the control strain. This clearly manifests that also in a system over-loaded with cells, separation to the detergent phase of cells expressing a hydrophobin on cell surface occurs.

Example 23**Partitioning of EGICore-HFBI fusion protein in hydrophobin-containing and non-containing pure systems**

5 The effect of free HFBI and HFBII hydrophobins on the partitioning of EGICore-HFBI was investigated by comparing how efficiently a sample of purified EGICore-HFBI in 50 mM acetate buffer pH 5.0 was extracted to the detergent phase in the presence and absence of purified HFBI and HFBII. The extraction was followed by measuring the depletion of hydrolytic activity on a soluble substrate such as methylumbelliferyl
10 cellobioside in the aqueous phase before and after extraction. When 0.7 g/l of either purified hydrophobin was present in the separation of 0.02 g/l of EGICore-HFBI with 2% C12-18EO5 at 30°C the extraction was affected in the following way: 93% of the protein was extracted when additional hydrophobin was not present, but with HFBII present 82% was extracted and with HFBI present 88% was extracted.

15

Example 24**Production of EGICore-HFBI fusion proteins in *T. reesei* $\Delta hfb2$ strain for improved partitioning of the fusion protein in ATPS**

20 *Trichoderma reesei* strain QM9414 $\Delta hfb2$ (VTT-D-99726) was transformed essentially as described (Penttilä *et al.*, 1987) using 10 µg of the plasmid pMQ113 (described in Example 1) together with 3 µg of the selection plasmid pTOC202 containing the *amdS* gene (Hynes *et al.*, 1983); Tilburn *et al.*, 1983) of *Aspergillus nidulans* encoding for acetamidase. pMQ113 contains an expression cassette for production of EGICore-HFBI fusion protein under the
25 control of *cbh1* promoter and terminator sequences.

The Amd⁺ transformants obtained were streaked two times onto plates containing acetamide (Penttilä *et al.*, 1987). Thereafter spore suspensions were made from transformants grown on Potato Dextrose agar (Difco). The production of the EGICore-HFBI fusion protein was
30 tested by slot blotting or Western analysis with EGI and HFBI specific antibodies from shake flask or microtiter plate cultivations carried out in minimal medium supplemented with Solka

flock cellulose. The spore suspensions of the clones producing fusion protein were purified to single spore cultures on selection plates containing acetamide. To determine the best producers, production of the fusion protein was analyzed again from these purified clones as described above.

5

For partitioning experiments of the EGCore-HFBI fusion protein in ATPS using the polyoxyethylene detergent C12-18EO5 the best production strain obtained in this study and as control strains VTT-D-98691 (QM9414 strain producing EGCore-HFBI) and VTT-D-74075 (QM9414) were cultivated in shake flasks on medium containing Solka flock cellulose as described in Example 4.

10

Standard partitioning experiments as described in Example 5 are carried out with culture supernatants. After separation the volume ratio of the lighter and heavier phase is noted and the concentration factor for the fusion protein is calculated from it. Samples are also taken from the lighter and heavier phase and analysed with SDS-PAGE, Western blotting and activity measurements as described in Example 5. Partition coefficients (K) and yields (Y) are calculated as described in Example 5.

15

Example 25

20 Construction of vectors for expression of EGCore-HFBI and EGCore-SC3 fusion proteins under the *cbh1* promoter of *T. reesei*

For construction of an expression vector for production of EGCore-HFBI fusion protein, *hfb2* (SEQ ID 20) coding region (from Ala-16 to the STOP codon) was amplified by PCR using phb2 (Nakari-Setälä et al. 1997) as a template and as a 5' primer **CGG AGG AGC TCG ACG ACT TCG AGC AGC CCG AGC TGC ACG CAG GCT GTC TGC CCT ACC GG** (SEQ ID 21) and as a 3' primer **TCA TTG GAT CCT TAG AAG GTG CCG ATG GC** (SEQ ID 22). The sequence is bold in the 5' primer encodes for amino acids 413-425 of EGI and the underlined GAGCTC is a SacI site. The underlined GGATCC in the 3' primer is a BamHI site. The amplified fragment was digested with SacI and BamHI and ligated to pMQI13 cut with the same restriction enzymes. The resulting plasmid is pTNS32

25

30

(Figure 18) and it carries the coding sequence for EGIcore-HFBII fusion protein under the control of *cbh1* regulatory sequences (SEQ ID 5 and SEQ ID 7).

For construction of an expression vector for production of EGIcore-SC3 fusion protein, SC3
 5 cDNA (SEQ ID 23) was amplified with PCR using cSC3/pUC20 plasmid as a template and as
 a 5' primer ACT ACA CGG AGG AGC TCG ACG ACT TCG AGC AGC CCG AGC
 TGC ACG CAG GGT GGC CAC CCG GGC (SEQ ID 24) and as a 3' primer TCG TAC
GGA TCC TCA GAG GAT GTT GAT GGG (SEQ ID 25). The sequence is bold in the 5'
 primer encodes for amino acids 413-425 of EGI and the underlined GAGCTC is a SacI site.
 10 The underlined GGATCC in the 3' primer is a BamHI site. The amplified fragment was
 digested with SacI and BamHI and ligated to pMQ103 (described in Example 1) cut with the
 same restriction enzymes. The resulting plasmid is pTH4 (Figure 19) and it carries the coding
 sequence for EGIcore-SC3 fusion protein under the control of *cbh1* regulatory sequences
 (SEQ ID 5 and SEQ ID 7).

15

The cSC3/pUC20 plasmid contains the 411 bp SC3 cDNA from the translational start site to
 the STOP codon in a pUC20 vector. The translational start site has been constructed to a
 NcoI site and a BamHI site has been added after the translational STOP codon.

20 Example 26

**Construction of a vector for expression of a HFBI-dCBD fusion protein containing
 hydrophobin I and double cellulose binding domains (CBD) under the *cbh1*
 promoter of *T. reesei***

25 For construction of an expression cassette for production of HFBI -dCBD fusion protein
 under *cbh1* promoter, the protein coding region of *hfbI* was amplified with PCR using
 pEA10 (Nakari-Setälä et al. Eur. J. Biochem. (1996) 235:248-255) as a template. GGA
 ATT CCG CGG ACT GCG CAT CAT GAA GTT CTT CGC CAT CGC C (SEQ ID
 26) was used as a 5' primer in the PCR and TGA ATT CCA TAT GTT AGG TAC CAC
 30 CGG GGC CCA TGC CGG TAG AAG TAG AAG CCC CGG GAG CAC CGA CGG
CGG TCT GGC AC (SEQ ID 27) as a 3' primer. The sequence in bold in the 5' primer
 is 16 bp of *cbh1* promoter adjacent to translational start site of the corresponding gene

and the underlined CCGCGG is a KspI site. The underlined and bold sequences in the 3' primer are NdeI and Asp718 sites, respectively. The sequence in *Italics* in the 3' primer encodes for a Methionine-containing linker (PGASTSTGMGPGG). The resulting fragment of 370 bp was digested with KspI and NdeI and ligated to pAMH110
5 (Nevalainen, K.M.H., Penttilä, M.E., Harkki, A., Teeri, T.T. and Knowles, J. (1991) In Molecular Industrial Mycology. Eds. Leong, S.A. and Berka, R., Marcel Dekker, New York) digested with same restriction enzymes. The resulting plasmid is pTNS29-2Asp.

For further cloning steps, an Asp718 site was removed from the pTNS29-2Asp
10 polylinker. The vector was digested with SacI and BamHI and the cleaved vector ends were blunted with T4 DNA polymerase and ligated together. The resulting vector pTNS29 is missing the SacI, Asp718 and SmaI sites present in the pTNS29-2Asp polylinker.

15 In the next step, a double cellose binding domain (dCBD) was amplified with PCR using pTNS11 as a template. pTNS11 carries the coding sequence for a fusion protein containing *T. reesei* CBHII CBD (41 N-terminal residues of CBHII) and CBHI CBD linked together via CBHI linker region (CBHI linker and CBD are the last 57 residues in CBHI). This DNA sequence originates from an *E. coli* expression vector B599 which is
20 essentially the same as the one described by Linder et al. (J. Biol. Chem. (1996) 271:21268-21272). TGA ATT CGG TAC CCA GGC TTG CTC AAG CGT C (SEQ ID 28) was used as a 5' primer in the PCR and TGA ATT CCA TAT GTC ACA GGC ACT GAG AGT AGT A (SEQ ID 29) as a 3' primer. The underlined sequences in the 5' and 3' primers are Asp718 and NdeI sites, respectively. The amplified fragment was digested
25 with Asp718 and NdeI and ligated to pTNS29 digested with Asp718 and NdeI resulting in pTNS30.

pTNS30 (Figure 20) expression vector thus carries the coding region for a fusion protein consisting of HFBI and double CBD linked in frame via the Methionine linker peptide
30 (PGASTSTGMGPGG). Expression of the fusion protein is regulated by the *cbhI* transcriptional control sequences. The expression cassette may be released from the plasmid with EcoRI and SphI.

Example 27**Construction of vectors for expression of HFBI-single chain antibody fusion proteins under the *cbh1* promoter of *T. reesei***

- 5 An expression vector was constructed for production of a fusion protein consisting of *T. reesei* HFBI protein in the N-terminus and in the C-terminus a single chain antibody recognizing a small molecular weight derivative of diarylalkyltriazole (ENA5ScFv). Production of the fusion protein is under the *cbh1* regulatory sequences. For construction of HFBI-ENA5ScFv fusion protein, pENA5ScFv was digested with NcoI and XbaI. The
- 10 fragment containing the *ena5scfv* gene and the histidine tail (6 x His) was blunt-end cloned to pTNS29 resulting in pTH1 (Figure 21). pENA5ScFv vector carries the coding region for ENA5 single chain antibody consisting of the variable domains of the heavy and light chains connected via a glycine serine linker and a 6 x histidine tag at the C-terminal end. Transcription and secretion of the single chain antibody are under control of the *tac* promoter
- 15 and *pelB* signal sequence, respectively (Takkinen *et al.*, 1991). pTNS29 vector carries the *hfb1* coding region of *T. reesei* followed by a linker sequence (ProGlyAlaSerThrSerThrGlyMetGlyProGlyGly) under the control of *cbh1* promoter and terminator sequences.
- 20 For construction of HFBI-ENA5ScFv fusion protein with a thrombin cleavage site in the linker peptide, *ena5scfv* coding region (from Ala-23 to the STOP codon) and a peptide linker containing the thrombin cleavage site (Gly Thr Leu Val Pro Arg Gly Pro Ala Glu Val Asn Leu Val) preceding it was amplified with PCR using pENA5ScFv as a template and as a 5' primer GAA TTC GGT ACC CTC GTC CCT CGC GGT CCC GCC GAA GTG AAC
- 25 CTG GTG (SEQ ID 30) and as a 3' primer TGA ATT CCA TAT GCT AAC CCC GTT TCA TCT CCA G (SEQ ID 31). The sequence in bold in the 5' primer encodes the first 6 N-terminal residues of ENA5SCFV. The sequence in italics is a thrombin cleavage site and underlined GGT ACC is an Asp718 site. The sequence in bold in the 3' primer encodes the 6 C-terminal residues of ENA5ScFv and the underlined CA TATG is a NdeI site. The 790 bp
- 30 PCR fragment was purified from agarose gel and ligated to pTNS29 resulting in pTH2 (Figure 22).

Example 28**Construction of a vector for production of class I hydrophobin SC3 of *Schizophyllum commune* in *Trichoderma reesei* for ATPS**

- 5 A *T. reesei* strain producing class I hydrophobin SC3 of *S. commune* was constructed. For that purpose an expression vector carrying the SC3 cDNA under the control of *hfb2* promoter and *hfb1* terminator of *T. reesei* was constructed.

The *hfb1* terminator (SEQ ID 32) was amplified with PCR using as a template pEA10
 10 (Nakari-Setälä et al. 1996) and as a 5' primer GAC CTC GAT GCC CGC CCG GGG TCA AG (SEQ ID 33) and as a 3' primer GTC GAC ATT TCA TTT TAC CCC CCT CG (SEQ ID 34). The underlined sequences in the 5' and 3' primers are SacI and Sall sites, respectively. The PCR fragment was cut with SacI and Sall so that the SacI site was blunted with Klenow. The fragment was cloned into cSC3/pUC20 (described in Example
 15 25) vector digested with Sall and BamHI where the BamHI was blunted with Klenow. In the next step, the *hfb2* promoter (SEQ ID 35) was amplified with PCR using as a template pTNS8 (Nakari-Setälä et al. 1997) and using as a 5' primer AAG CTT GCA TGC CTG CAT CC (SEQ ID 36) and as a 3' primer CCA TGG TGA AAG GTG GTG ATG GTT GG (SEQ ID 37). The underlined sequences in the 5' and 3' primers are HindIII and
 20 NcoI sites, respectively. The PCR fragment was digested with HindIII and NcoI and cloned in front of the SC3 cDNA in the plasmid obtained in the previous step and cut with the same restriction enzymes. The resulting plasmid is pKS2 (Figure 23).

Example 29

- 25 **Construction of *T. reesei* strains producing EGCore-HFBII, EGCore-SC3, HFBI-dCBD and HFBI-single chain antibody fusion proteins, and SC3 hydrophobin**

Trichoderma reesei strains VTT-D-74075 (QM9414), VTT-D-86271 (Rut-C30) and VTT-D-99676 (Rut-C30 $\Delta hfb2$) were co-transformed essentially as described (Penttilä et al.,
 30 1987) using 3-13 μ g of the plasmids pTNS32, pTH1, pTH2, pTH4, pTNS30 and pKS2 and as the selection plasmids 1-3 μ g pToC202 or pARO21. pToC202 carrying the *amdS* gene (Hynes et al., 1983; Tilburn et al., 1983) of *A. nidulans* and pARO21 carrying the *E. coli hph*

gene have been described in Example 3. The Amd⁺ and Hyg⁺ transformants obtained were streaked three times onto plates containing acetamide and hygromycin, respectively (Penttilä *et al.*, 1987). Thereafter spore suspensions were made from transformants grown on Potato Dextrose agar (Difco).

5

The production of the fusion proteins EGIcore-HFBII, EGIcore-SC3, HFBI-dCBD and HFBI-ENA5ScFv and the SC3 hydrophobin was tested by slot blotting or Western analysis with EGI, SC3, CBD and HFBI specific antibodies from shake flask or microtiter plate cultivations carried out in minimal medium supplemented with either lactose or Solka flock
10 cellulose. The spore suspensions of the fusion protein producing clones were purified to single spore cultures on selection plates (containing either acetamide or hygromycin). To determine the best producers, production of the fusion proteins was analyzed again from these purified clones as described above.

15 *T. reesei* strains selected for further cultivations are X46A (pTNS32, host QM9414), VTT-D-00793 (pTH4, host Rut-C30 $\Delta hfb2$), VTT-D-99727 (pTNS30, host Rut-C30 $\Delta hfb2$), VTT-D-00791 (pTH1, host Rut-C30) and VTT-D-00792 (pKS2, host Rut-C30 $\Delta hfb2$). These strains were cultivated as described in Example 4 and the culture supernatants were subjected to ATPS.

20

Example 30

Recovery of the protein product from the enriched detergent phase after ATPS by isobutanol or other solvents

25 After phase separation has occurred and the hydrophobin or the hydrophobin fusion protein is enriched in the detergent phase (the enriched phase), the protein can be recovered to an aqueous buffer by addition of isobutanol or other solvent. For example a series, of identical extractions of 0.05 g/l HFBI in 50 mM acetate buffer was made with 2% Berol 532. To separate tubes 10% final concentration of either isobutanol, n-amyl
30 alcohol, octanol, or octane was added. and the fraction of hydrophobin recovered to the aqueous phase was analyzed. It was found that 100% was recovered with isobutanol,

89% with n-amyl alcohol, 81 % with octanol and 70 % with octane. Fractions were analyzed by HPLC as described in Example 38.

5 **Example 31**

Separation of EGICore-HFBII fusion protein in ATPS.

T.reesei strain X46A was grown in shake flasks on 3% lactose medium as described in Example 4. C12-18EO5 detergent was added to a final concentration of 5% to the culture supernatant. After mixing the system was allowed to settle and the enriched
10 detergent phase was subjected to further extraction with an equal volume of isobutanol. After buffer exchange on Biogel P-6 (Bio-Rad, USA) gel filtration media, the extracted protein was analysed by ion exchange chromatography using a Mono Q (Amersham Pharmacia, Sweden) column equilibrated with 15 mM acetate and eluted using a linear gradient of NaCl. Separation of the EGICore-HFBII fusion protein to the detergent phase
15 was verified by analyzing the eluted peak fraction from the Mono Q chromatography run by its activity on 4-methylumbelliferyl cellobioside as well as its re-extraction by ATPS.

Example 32

Separation of EGICore-SC3 fusion protein in ATPS

20

Culture filtrate of *T.reesei* strain VTT-D-00793 producing EGICore-SC3 fusion protein was subjected to APTS by adding 5% final concentration of C12-18EO5. After the settling, the phases were separated and the fusion protein enriched detergent phase was further treated with an equal volume of isobutanol which removes the detergent to the
25 isobutanol and leaves the protein in the aqueous phase. The resulting fusion protein enriched aqueous phase was then desalted on Biogel P-6 (Biorad, USA). Separation of fusion protein to the detergent phase was verified by analyzing the enzymatic activity of the EGICore fusion partner on 4-methylumbelliferyl cellobioside in that phase.

30

Example 33**Separation of HFBI-dCBD fusion protein in ATPS**

T.reesei strain VTT-D-99727 producing HFBI-dCBD fusion protein was grown on
5 lactose-containing medium as described in Example 4. Berol 532 was added to a final
concentration of 2 % to 500 ml of culture supernatant. The mixture was allowed to settle
and the phases separated in a separation funnel. The enriched top phase (10 ml) was
extracted with an equal volume of isobutanol and 50 mM acetate buffer pH5. The fusion
protein was selectively enriched to the buffer in the separation as shown by SDS gel
10 electrophoresis (Figure 24).

Example 34**Recovery of the HFBI-dCBD fusion partners after chemical cleavage**

15 HFBI-dCBD protein produced by the strain VTT-D-99727 has a methionine
(PGASTSTGMGPGG) designed in the linker region between the HFBI and the dCBD,
which would enable the recovery of the native HFBI and dCBD after chemical cleavage with
CNBr.

20 The HFBI-dCBD fusion protein was purified as described in Example 33. The resulting water
phase (~108 ml) still contained a small amount of CBHI and free hydrophobin in addition to
the HFBI-dCBD fusion (Figure 24). Further purification of the sample was performed by
chromatography. The sample was desalted on a Biogel P-6 column equilibrated with 50mM
sodium acetate buffer pH 5.5, diluted 1 + 3 with water and applied on a CM-Sepharose FF
25 column equilibrated with 10mM sodium acetate buffer pH 5.5. The CBHI protein was found
in the flow through and the purified HFBI-dCBD protein was eluted with 0.2M NaCl.

A sample of purified HFBI-dCBD protein was evaporated in speed-vac almost to dryness.
CNBr cleavage was performed by adding a solution of CNBr in 0.1M HCl (5mg/ml) to the
30 evaporated sample in 5 times weight excess. The reaction was allowed to continue for 24h at
room temperature (in dark). A 10 times volume of water was added and the sample was

evaporated in speed-vac almost to dryness. The evaporated sample was diluted in 50mM Tris-HCl pH 7 and the cleavage was confirmed by HPLC analysis as described in Example 37.

- 5 The treatment was further optimised by using different concentrations of HCl and incubation times. The final CNBr treated sample was subjected to ATPS as described in Example 33. HFBI was found in the top-phase and the dCBD in the bottom phase, thus leading to a separation of both fusion partners.

10 **Example 35**

Separation of HFBI-single chain antibody fusion protein in ATPS

- Strain VTT-D-00791 was cultivated for 7 days on medium containing 10 g/l potassium phthalate, 15 g/l KH_2PO_4 , 5 g/l $(\text{NH}_4)_2\text{SO}_4$ and 3% lactose and 0.2% peptone. 30 ml of
- 15 culture medium was subjected to ATPS using 4% C12-18-EO5 detergent as described in Example 5. After removal of the bottom phase, the detergent phase was extracted by isobutanol. Proteins from the water phase after detergent extraction and the bottom phase of the isobutanol extracted detergent phase were precipitated with trichloroacetic acid (final concentration 10%), resuspended in SDS-PAGE sample buffer (taking into account the
- 20 concentration factor of the isobutanol extracted detergent phase) and analysed by Western blotting using HFBI specific antibodies. The fusion protein runs as a dimer (approximately 70 kDa) in SDS-PAGE under the conditions used as seen in Figure 25. The water phase sample still contained a small amount of fusion protein. Nevertheless, separation of the fusion protein can be obtained by ATPS.

25

Example 36

Separation of SC3 hydrophobin in ATPS

- SC3 hydrophobin producing strain VTT-D-00792 was cultivated in shake flasks on lactose-
- 30 containing medium as described in Example 4. Soluble secreted proteins produced by the fungus were precipitated with trichloroacetic acid. Precipitated proteins were solubilized in trifluoroacetic acid to dissociate the SC3 aggregates whereafter the acid was evaporated with

a stream of air. The treated proteins were solubilized in 2 ml water containing 2.5 % of the detergent C12-18EO5. Phase separation was carried out as described in Example 5. Samples were taken from the lighter and heavier phase and analysed by Western blotting using SC3 specific antibodies. On the basis of this analysis, SC3 hydrophobin partitions to the detergent
5 phase (Figure 26).

Example 37

Separation of nisin in ATPS

10 1 mg of pure nisin (Sigma) (equals to 1000 IU) in 50 mM sodium acetate buffer pH 5 was subjected to ATPS using 2% of the detergent C12-18EO5 at 30°C, and the phases were allowed to settle. After removal of the bottom phase, the detergent phase was extracted by isobutanol which removes the detergent to the isobutanol and leaves nisin in the aqueous phase. Separation of nisin to the enriched aqueous phase was assayed testing nisin
15 bioactivity as described by Qiao et al. 1996. Comparison of the halos on the assay plate produced by the enriched phase and the nisin controls indicated that nisin had separated to the detergent phase with a concentration factor of approximately 5.

20 Example 38

Preparative purification of HFBI and HFBII in ATPS

For preparative purposes, HFBI and HFBII were extracted from 0.5 l of culture supernatants from cultivations carried out on media containing glucose or cellulose as
25 described in Example 4. 2% (w/w) detergent was added to the culture supernatant which was mixed and then allowed to settle in a separation funnel at 20°C if C11EO2 (Berol 532) was used and 30°C if C12-18EO5 (Henkel) was used. The detergent phase (enriched phase) was collected and mixed with an equal volume of isobutanol. When C11EO2 was used an equal volume of 50 mM acetate buffer was also added. The
30 remaining culture supernatant is the depleted phase. To follow the purification, analytical HPLC was run on samples from each step (Figure 27 and 28). On the basis of HPLC analysis, both HFBI and HFBII partitioned well to both of the detergents. When

C11EO2 was used, K values of >1000 and >78 were obtained for HFB I and HFB II, respectively.

Water phase after isobutanol extraction was collected and further purified on a Vydac
5 Ix20 cm semipreparative C4 column (Vydac, USA) equilibrated with 0.1% trifluoro acetic acid in water and eluting with a linear gradient of 0.1% trifluoro acetic acid in acetonitrile. The proteins were then lyophilized. In analytical runs a 4.6 mmx20 cm Vydac C4 column was used.

10 **Example 39**

Screening for separation conditions using purified HFB I and HFB II

HFB I and HFB II which were purified from culture supernatants in ATPS, further purified by preparative HPLC and lyophilized as described in Example 38 were dissolved
15 in water to a concentration of 0.5 mg/ml. The stock solutions were then diluted with the buffer appropriate for the experiment. 50 mM acetate buffer pH5, 50 mM glycine pH 3, 50 mM HEPES pH 7 was used for pH screening and NaCl or $(\text{NH}_4)_2\text{SO}_4$ in acetate buffer was used for ionic strength experiments. The surfactant was weighed with the appropriate amount of hydrophobin solution and incubated in 0, 20, 30, 40°C and the
20 amount of hydrophobin in the depleted phase determined. Partitioning coefficients were calculated from the change in concentration and the volume ratios and are presented in the tables below.

25

30

Table presenting K-values for the separation of hydrophobins with different surfactants and temperature.

	Temperature	Henkel	Berol 532	Berol 266	Triton x114
HFBI	0°C	0,1	368	NP	NP
	20°C	0,4	1961	NP	NP
	30°C	85	2970	NP	0,9
	40°C	148	682	28	69
HFBII	0°C	NP	76	NP	NP
	20°C	1,0	139	NP	NP
	30°C	67	194	NP	4,0
	40°C	44	102	19	44

5 NP = no phase separation

Table presenting the effect of different salt concentrations at 40°C on K-values

10

		Henkel	Berol 532	Berol 266	Triton x114
HFBI	50 mM buffer	244	578	13	39
	+ 1 M NaCl	239	33	198	241
	+1 M (NH ₄) ₂ SO ₄	0,9	3,2	176	612
HFBII	50 mM buffer	36	80	16	58
	+ 1 M NaCl	14	87	61	38
	+1 M (NH ₄) ₂ SO ₄	3,1	351	95	35

Table presenting the K-values for the partitioning of hydrophobins in Berol 532 at different conditions.

15

	HFBI 0°C	HFBI 20°C	HFBII 0°C	HFBII 20°C
50 mM acetate pH5	298	614	76	127
+1 M NaCl	614	3781	131	199
+1M (NH ₄) ₂ SO ₄	931	44	203	139
pH3	614	1881	73	160
pH7	361	614	54	126

Example 40**Purification of a new putative *T. reesei* hydrophobin on the basis of its separation in ATPS, and cloning of the corresponding gene**

5 *T. reesei* strain VTT-D-99726 (QM9414 $\Delta hfb2$) was cultivated on lactose-based medium in 15 fermentor as described in Example 4. After cultivation, 1 l of the culture filtrate was subjected to ATPS with 5% polyoxyethylene detergent C12-18EO5. After phase separation at 30°C, detergent phase was separated from the depleted aqueous phase and analysed by SDS-PAGE. The analysed sample contained a protein which
10 was about 7.5 kDa. In addition, some larger proteins were present. These were removed by hydrophobic interaction chromatography on a Phenyl-Sepharose FF column equilibrated with 50 mM sodium acetate - 1 M $(\text{NH}_4)_2\text{SO}_4$ buffer. The proteins were eluted with descending $(\text{NH}_4)_2\text{SO}_4$ salt gradient. Fractions containing the ca. 7.5 kDa protein were pooled and concentrated, and analysed by mass
15 spectrometry. This revealed that the purified protein was degraded to three peptides (2486, 2586 and 2709 Da), which were held together by disulphide linkages. The N-terminal amino acid sequence from the 2486 Da peptide was ANAFCPEGLLYTNPLCCDLL, which on the basis of position of cysteines and on sequence comparison to known hydrophobins is typical to a hydrophobin.

20

Degenerated primers were designed on the basis of this amino acid sequence as well as on the basis of the sequence obtained from the 2586 Da peptide. These primers were used in RT-PCR (RobusT RT-PCR Kit, Finnzymes) with RNA isolated from the same cultivation from where the protein was purified. The 140 bp fragment obtained
25 from the RT-PCR reaction was sequenced. The obtained sequence contained a part that was coding for the 2486 Da peptide used to design the PCR primer confirming that the PCR product corresponds to the purified protein.

30

Example 41**Purification of EGCore-HFBI in ATPS in pilot scale**

The strain VTT-D-99702 producing EGCore-HFBI fusion under the *cbh1* promoter was
5 cultivated in pilot scale fermentor in 1200 L on minimal medium containing 4% lactose,
0.4 % peptone and 0.1% Yeast Extract for 4 days. Cultivation temperatures were 28°C
or alternatively the temperature was changed during the cultivation from 27°C to 22°C in
a step-wise manner. Production level of the fusion protein was a few grams per liter.
After the end of the cultivation, the mycelium was separated by means of a rotating
10 vacuum drum filter using Celite 535 diatomaceous earth as filter aid.

In separation 1, 1100 L of the supernatant was transferred into the meanwhile cleaned
bioreactor, adjusted to the separation temperature of 24,7 °C and mixed with salt and
detergent to give 0,15 M ammonium dihydrogen phosphate and 4,1 % of detergent C12-
15 18EO5. The phases were left to separate by gravity settling and the heavier phase
removed through the bottom valve. A parallel experiment in 10 ml volume was carried
out to investigate the effect of scale up on the separation of the fusion protein. The
partition coefficient and the concentration factor were equal for the 10 ml and 1200 L
separation within the measurement error. The separated detergent phase was re-
20 extracted using the detergent phase from the first extraction by replacing half of the
volume of the bottom phase by tap water. The salt concentration was adjusted to 0,25 M
ammonium dihydrogen phosphate at 30°C. K and Y values of the separations are
presented in the below Table.

25 Alternatively in separation 2, 10 ml of drum filtrated culture medium samples were
subjected to ATPS at 25°C using 4.1% C12-18EO5 detergent and 1.15 M $(\text{NH}_4)\text{H}_2\text{PO}_4$.
K and Y values after one separation step are presented in the Table below.

30

35

Table presenting extraction experiments of culture supernatants from different pilot scale cultivations

Separation	Cultivation temperature	Concentration factor	K	Y [%]
Separation 1	27°C → 22°C	3.4	3.8	59
Re-extraction			8	70
Separation 2	29°C	2.8	8.3	81

5

Example 42

Separation of EGI, EGICore-HFBI fusion protein and HFBI hydrophobin in robust micelle/polymer systems

- 10 Separations were performed with purified samples. HFBI was purified by two-phase separation and HPLC as described in Example 38. EGICore-HFBI was purified by two-phase extraction as described in Example 5 followed by desalting on a Biogel P-6 column equilibrated with 20mM sodium acetate buffer pH 6 containing 150mM NaCl. The purified proteins were subjected to ATPS using different micelle/polymer systems.

15

- The table below presents partitioning coefficients of pure EGI, HFBI and EGICore-HFBI at constant tie-line length, in the different systems, Triton X-114/water system (4.1 % wt.) at 31.5° C, Triton X-100/Reppal/water system (8.1 % wt. / 8.2 % wt.) and Triton X-114/Reppal/water system (5.0 % wt. / 4.0 % wt.) at 21° C. The standard deviation is shown within the brackets. The systems were buffered with 25 mM sodium acetate, pH 4.0. $K > 1$ is equivalent to a preferred protein partitioning to the micelle rich phase.

20

	EGI	HFBI	EGICore-HFBI	
	K_{EGI}	K_{HFBI}	$K_{EGICore-HFBI}$	Yield (%) top phase
Triton X-114	0.6 (0.1)	21.5 (1.5)	8.4 (1.0)	85
Triton X-100/Reppal	0.9 (0.1)	-	1.7 (0.1)	56
Triton X-114/Reppal	0.7 (0.1)	11.0 (1.1)	15.4 (2.9)	91

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Claims

1. A process for partitioning of proteins or cells in aqueous two-phase systems (ATPS), comprising the steps of
 - 5 a) in order to obtain a fusion protein or cell, combining a protein or a cell of interest to a targeting protein selected from the group consisting of amphipathic and hydrophobic proteins having the ability to partition in ATPS and to carry said protein or cell of interest into one of the phases, and
 - b) 10 subjecting said fusion protein or cell carrying the targeting protein to an ATPS separation.
2. The process according to claim 1, wherein the targeting protein is a hydrophobin or hydrophobin-like protein or a part thereof.
- 15 3. The process according to claim 2, wherein the hydrophobin is a *Trichoderma* hydrophobin or a part thereof.
4. The process according to claim 3, wherein the *Trichoderma* hydrophobin is HFB1, HFBII or SRHI, or a part thereof.
- 20 5. The process according to claim 1, wherein the amphipathic or hydrophobic proteins or parts thereof form aggregates.
6. The process according to any one of claims 1 to 5 for partitioning cells in ATPS, wherein in step a) of claim 1 the combination of the cells of interest to the targeting protein 25 comprise bringing said targeting protein onto the surface of said cells.
7. The process according to claim 6, wherein the cells are yeast cells.
- 30 8. The process according to claim 6 wherein the cells are spores.
9. The process according to any one of claims 6 to 8, wherein the targeting protein is fused to a protein which brings the targeting protein onto the surface of the cell.

10. A fusion protein, comprising a hydrophobin or hydrophobin-like protein as defined in any one of claims 2 to 5 fused to a protein of interest.
11. The fusion protein according to claim 10, wherein the protein of interest is a cell-bound protein or a part thereof.
12. The fusion protein according to claim 10, wherein the protein of interest is an extracellular protein or a part thereof.
13. The fusion protein according to claim 12, wherein the extracellular protein is an extracellular protein of *Trichoderma*, selected from the group consisting of cellulases, hemicellulases and proteases.
14. The fusion protein according to claim 10, wherein the protein of interest is an antibody protein or a part thereof.
15. The process according to claim 1, wherein the targeting protein is fused to the protein of interest according to any one of the claims 10 to 14.
16. A recombinant organism producing a fusion protein according to any one of claims 10 to 14.
17. The recombinant organism according to claim 16, wherein the organism has been genetically modified to be capable of producing a fusion protein according to any one of claims 10 to 14.
18. A recombinant DNA molecule, comprising a DNA molecule encoding a fusion protein according to any one of claims 10 to 14.
19. A process for producing a fusion protein according to any one of the claims 10 to 14 with recombinant organisms, comprising the steps of
- a) transforming the organism with DNA molecules enabling expression of such proteins, and

b) recovering such protein from the culture of the recombinant organism.

20. The process according to any one of claims 1 to 9 and 15, wherein the aqueous two-phase system is selected from the group consisting of PEG/salt, PEG/Dextran and
5 PEG/starch systems or derivatives thereof, detergent-based aqueous two-phase systems and thermoseparating polymer systems.

21. The process according to claim 20, wherein the detergent-based ATPS comprises a detergent which is selected from the group consisting of nonionic and zwitterionic
10 detergents.

22. The process according to claim 20, wherein the thermoseparating polymer system comprises a polymer which is selected from the group consisting of polyethylene-polypropylene copolymers.

15

23. The process according to any one of claims 1-9 and 15, wherein the protein or cell of interest is separated from a suspension containing cells or cell extracts.

24. A process for separating hydrophobins or hydrophobin-like proteins or parts thereof
20 in aqueous two-phase systems, comprising the steps of

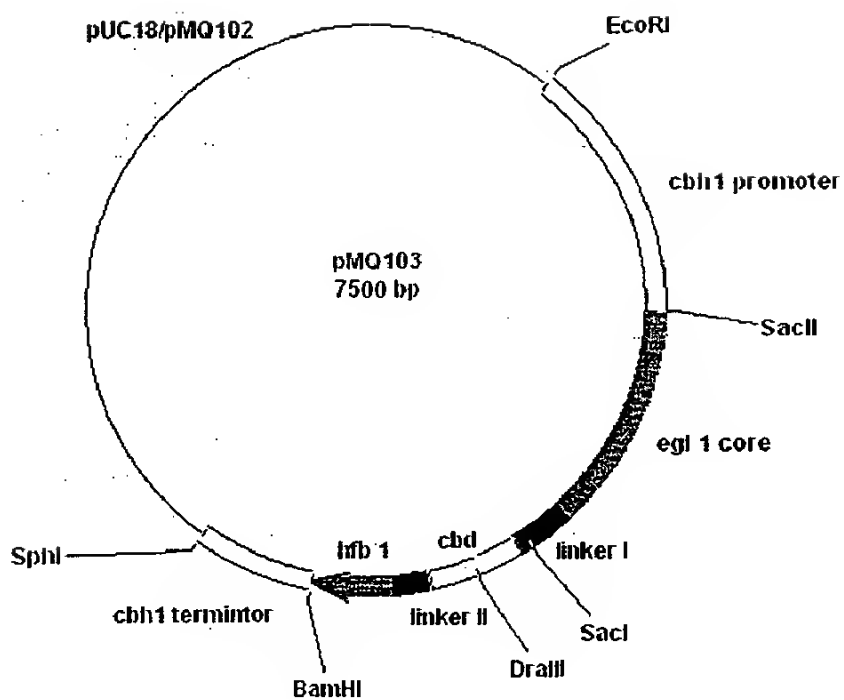
a) mixing solutions containing said hydrophobin, hydrophobin-like protein or parts thereof with the phase forming chemicals, and

b) carrying out ATPS separation,

wherein the aqueous two-phase system is as defined in any one of claims 20 to 22.

25

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**Fig 1.**

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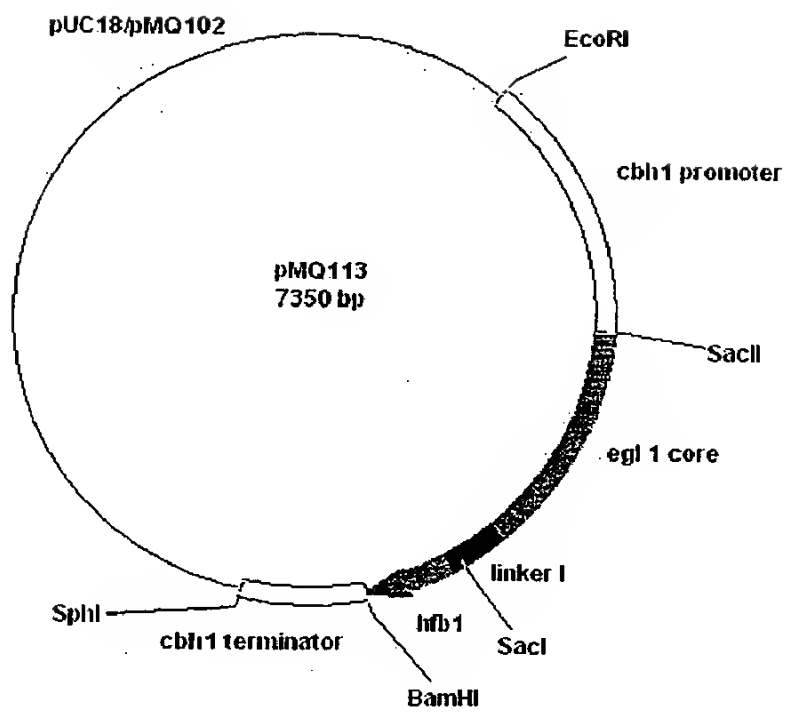


Fig 2.

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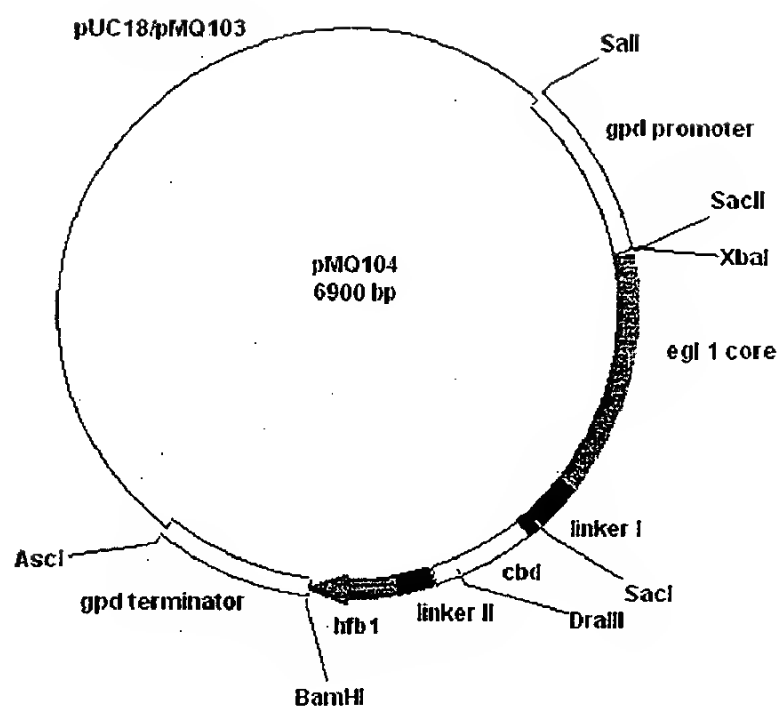


Fig 3.

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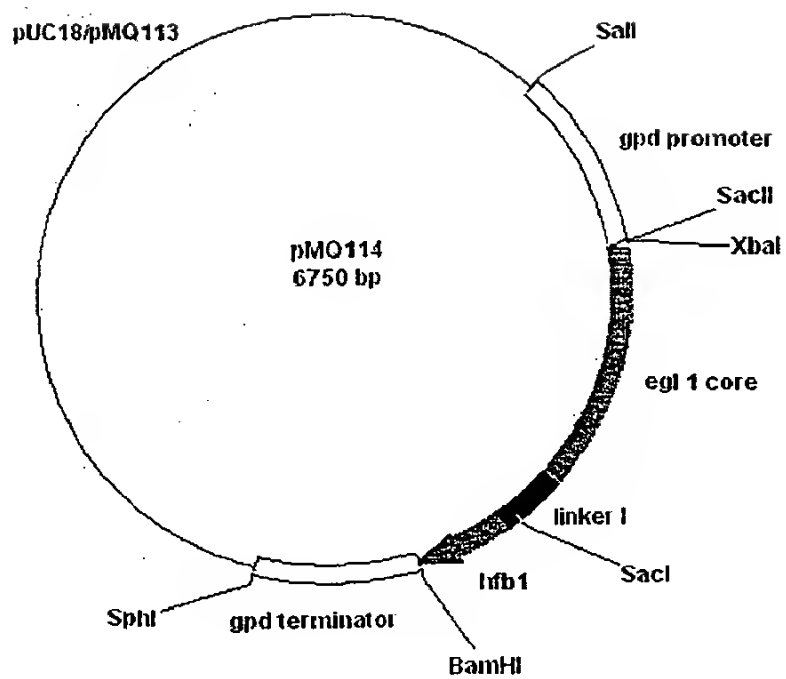


Fig 4.

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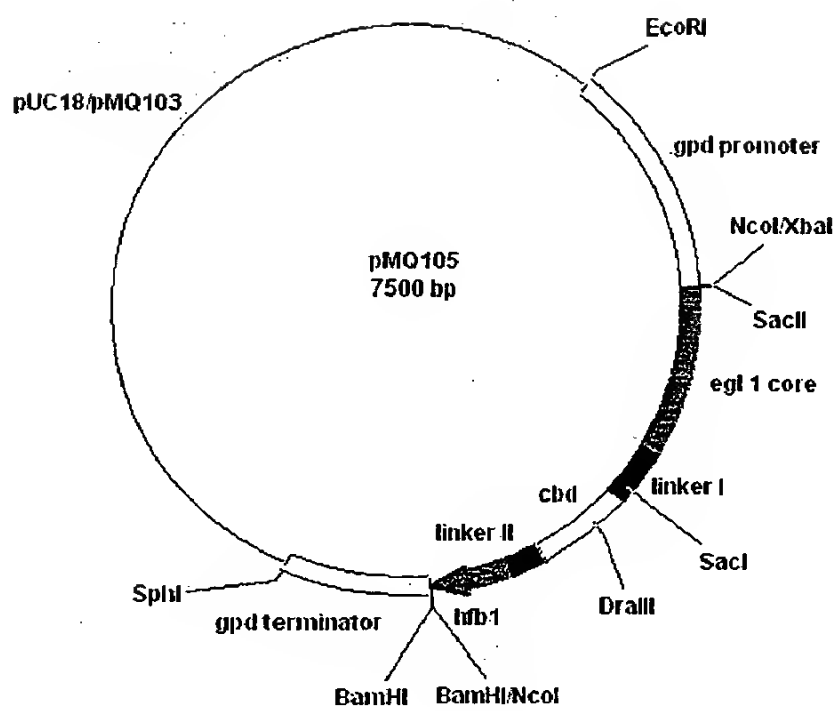


Fig 5.

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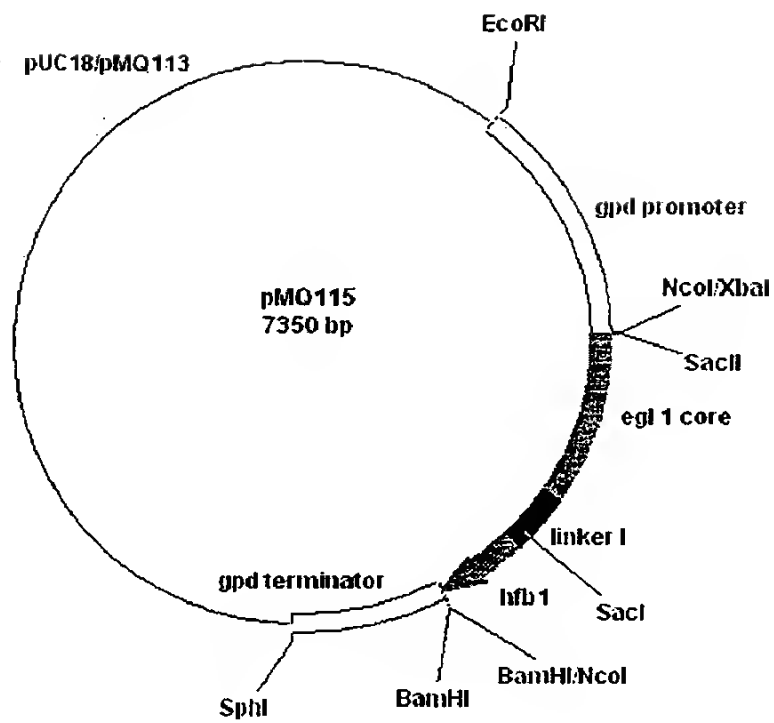
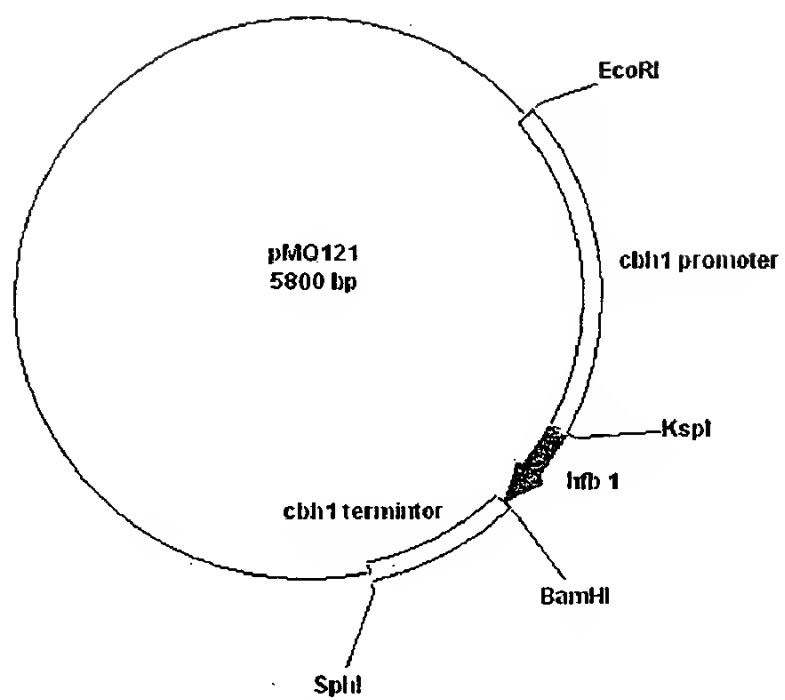


Fig 6.

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**Fig 7.**

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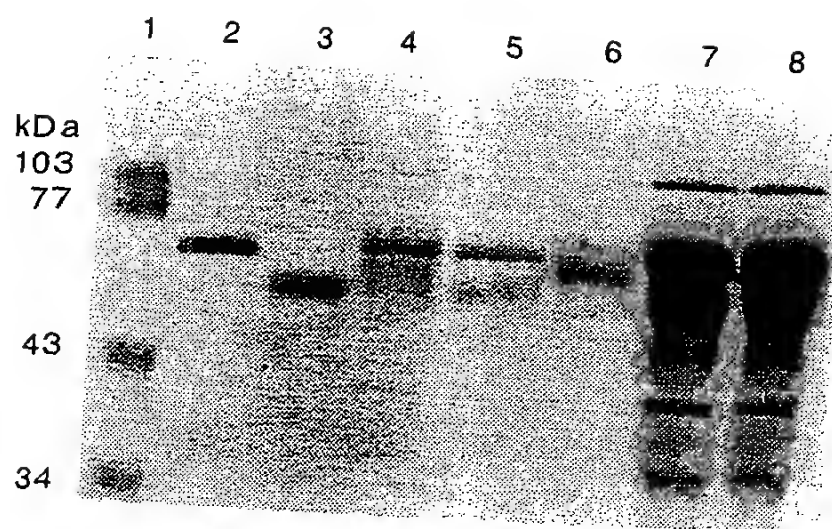


Fig. 8

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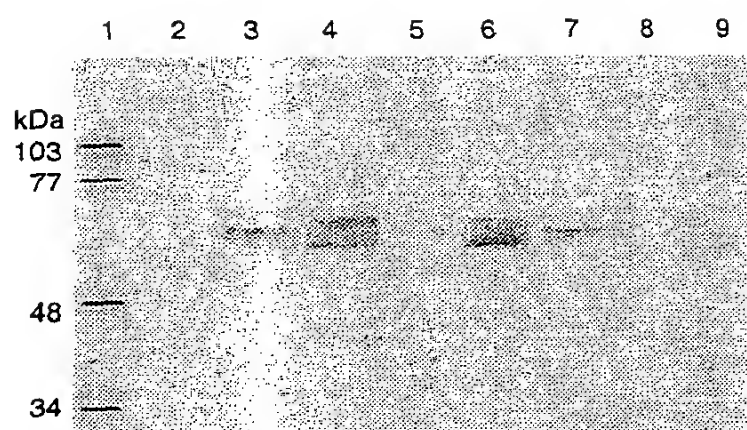


Fig. 9

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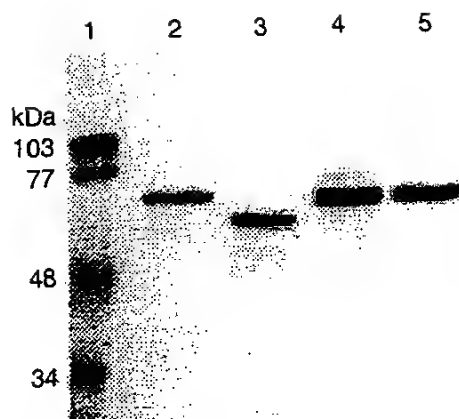


Fig. 10

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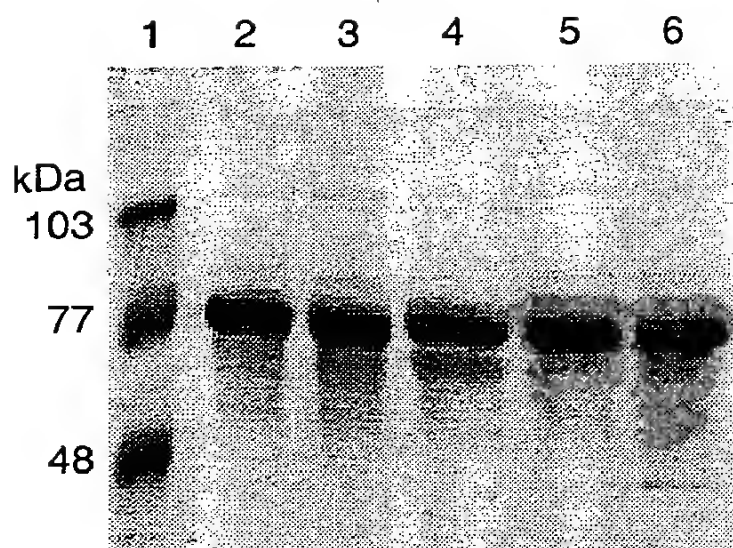


Fig. 11

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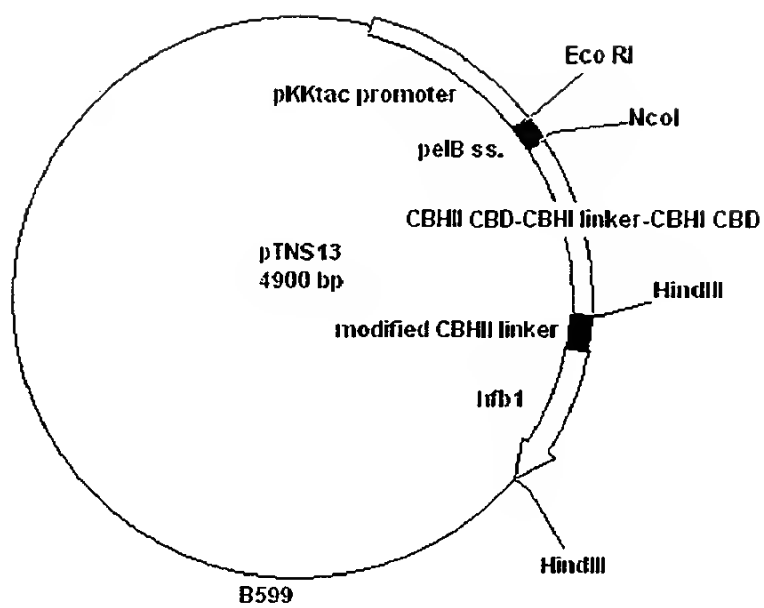


Fig 12.

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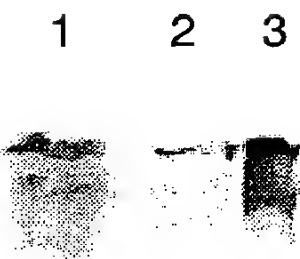


Fig. 13

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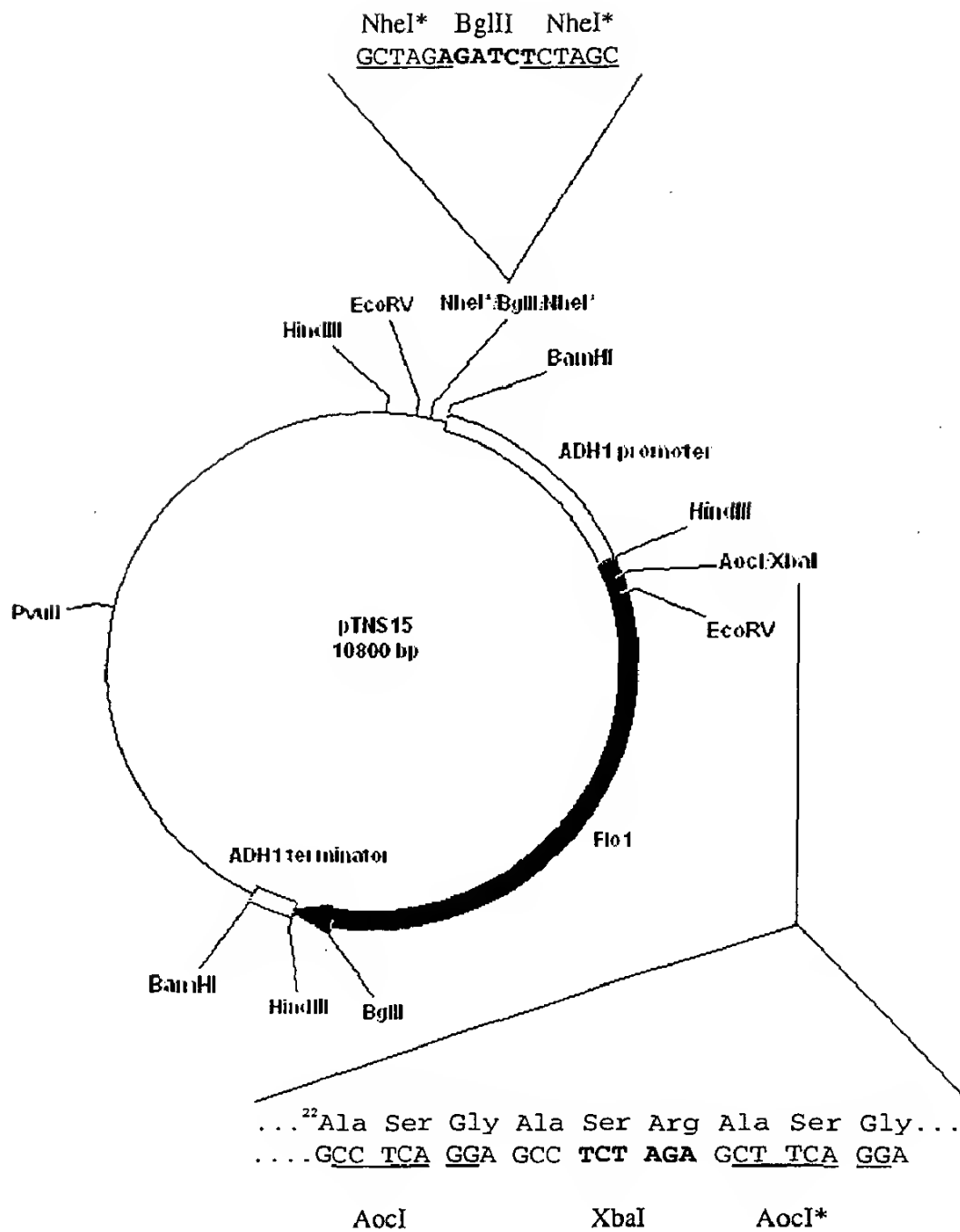


Fig 14.

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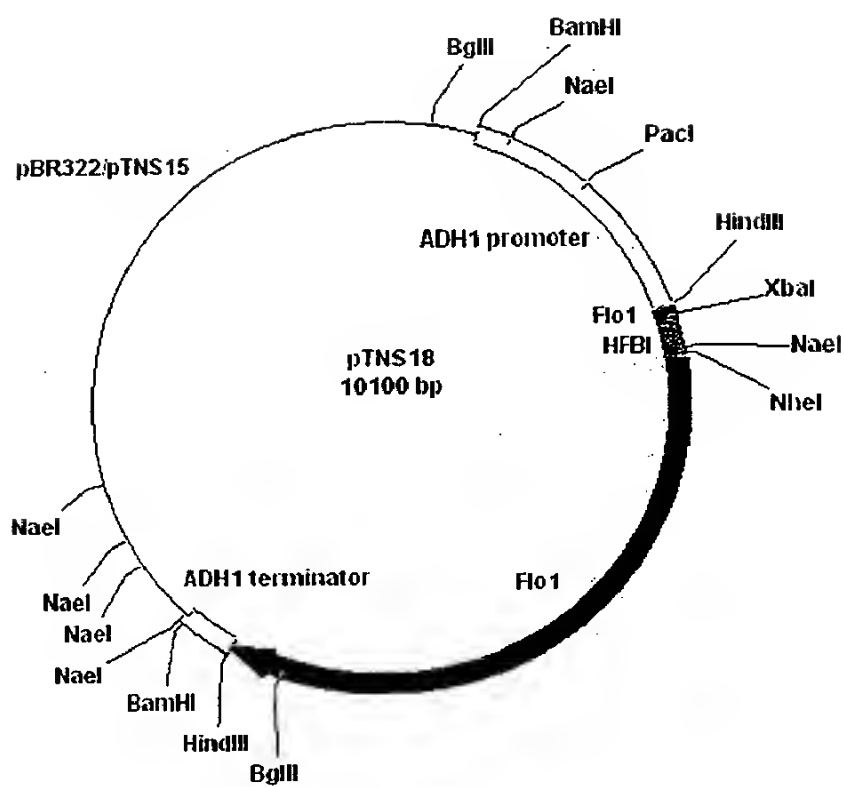


Fig 15.

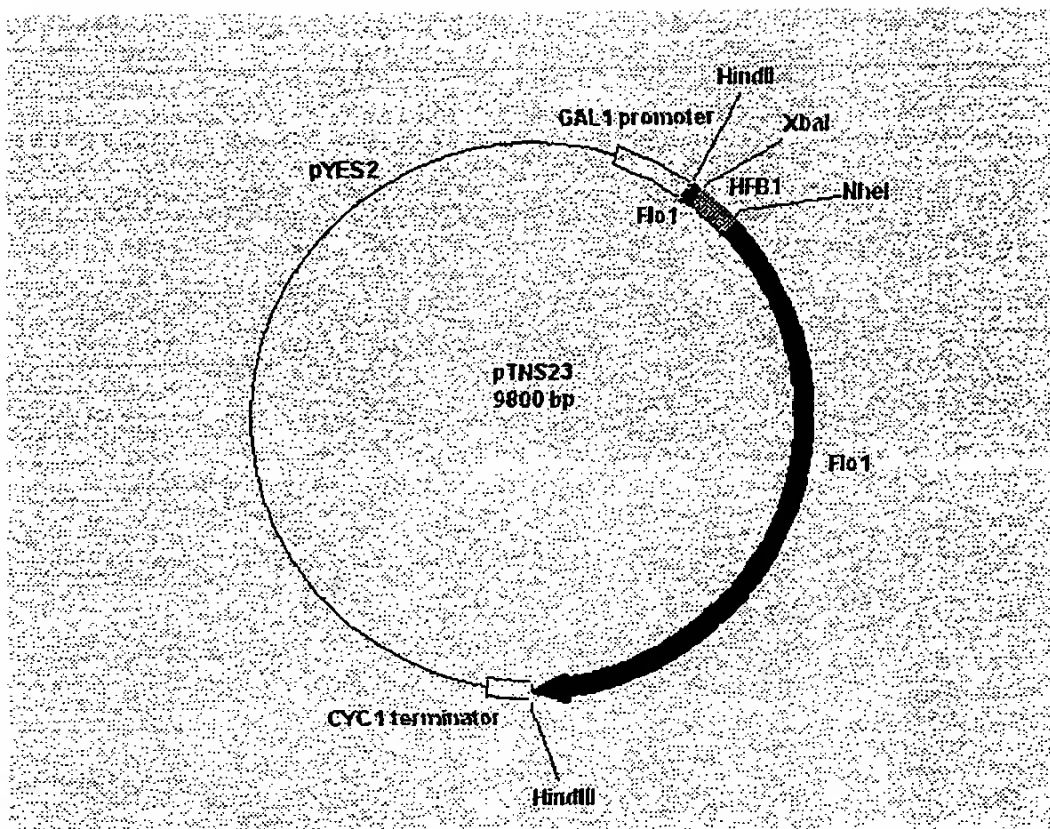


Fig. 16

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Fig. 17

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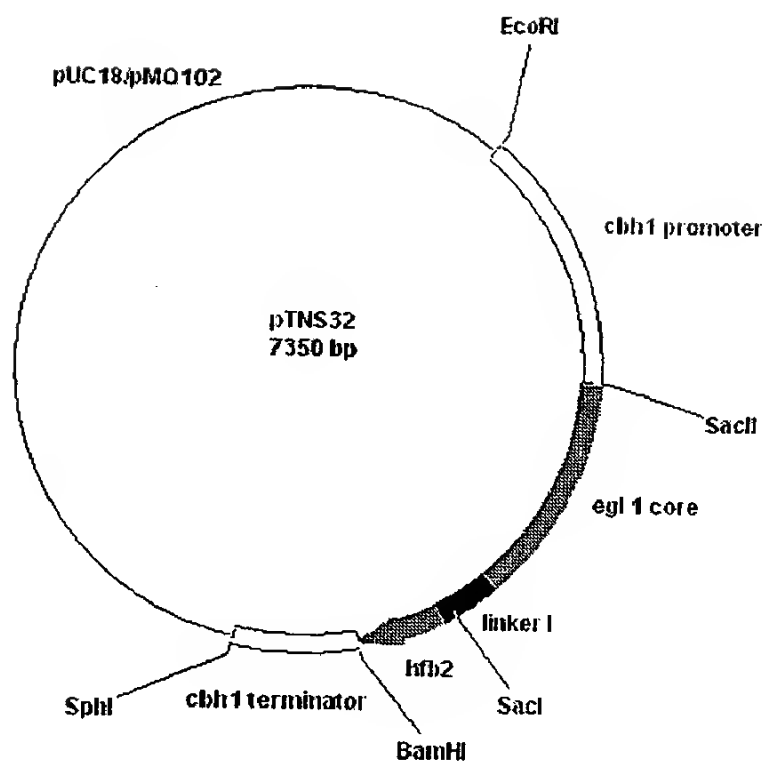


Figure 18.

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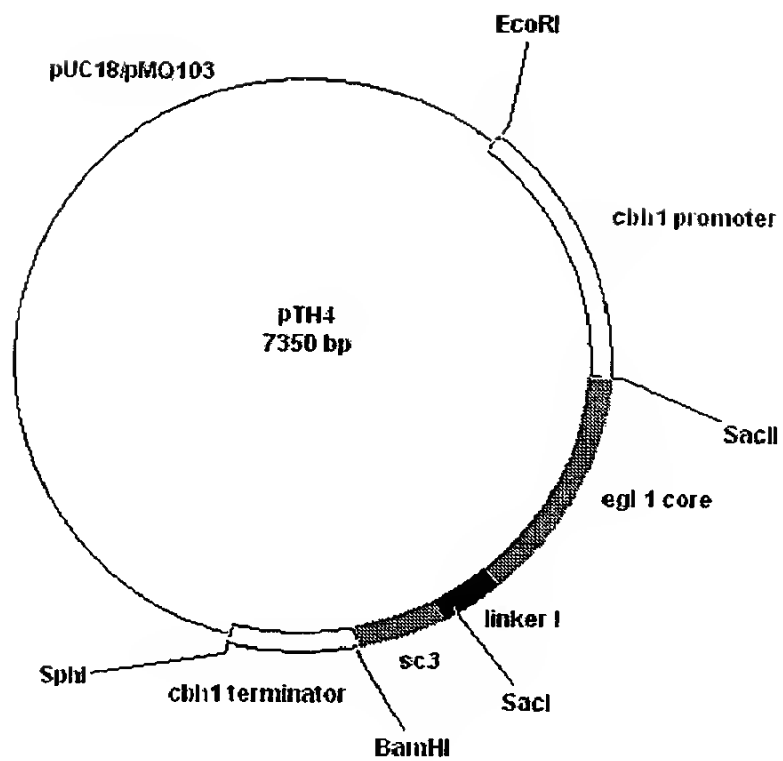


Figure 19

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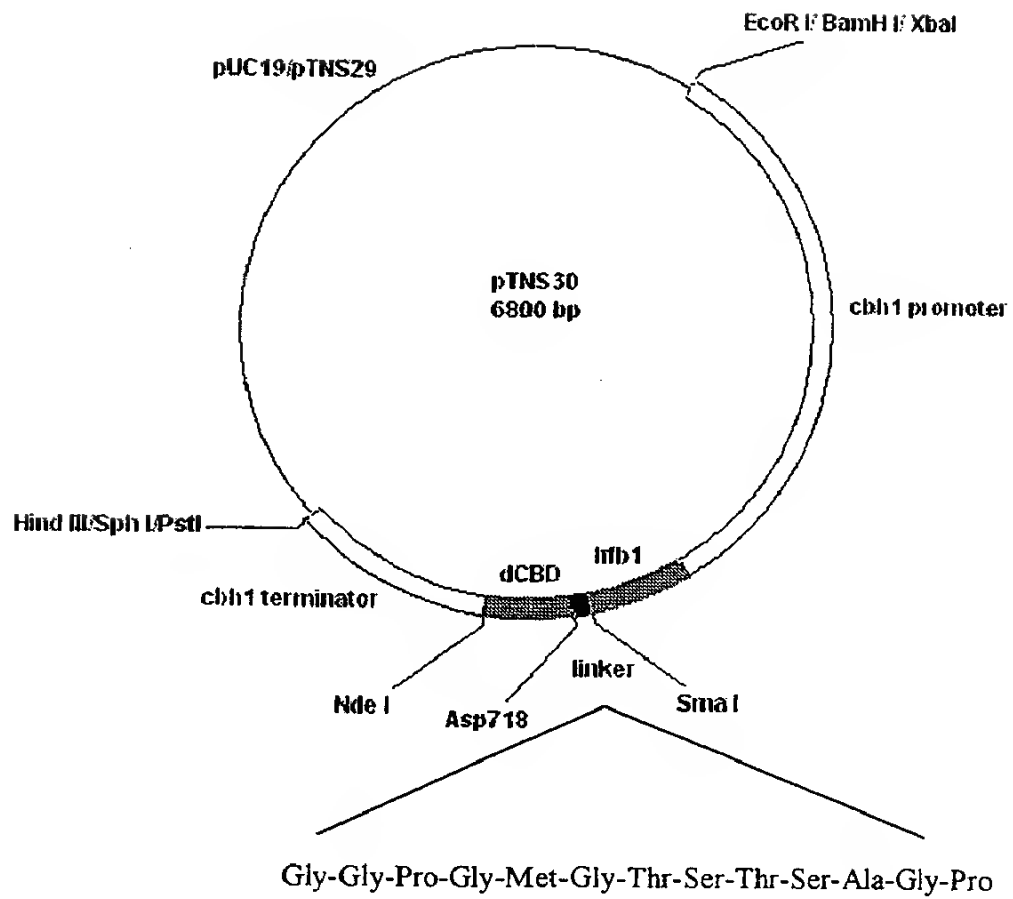


Figure 20.

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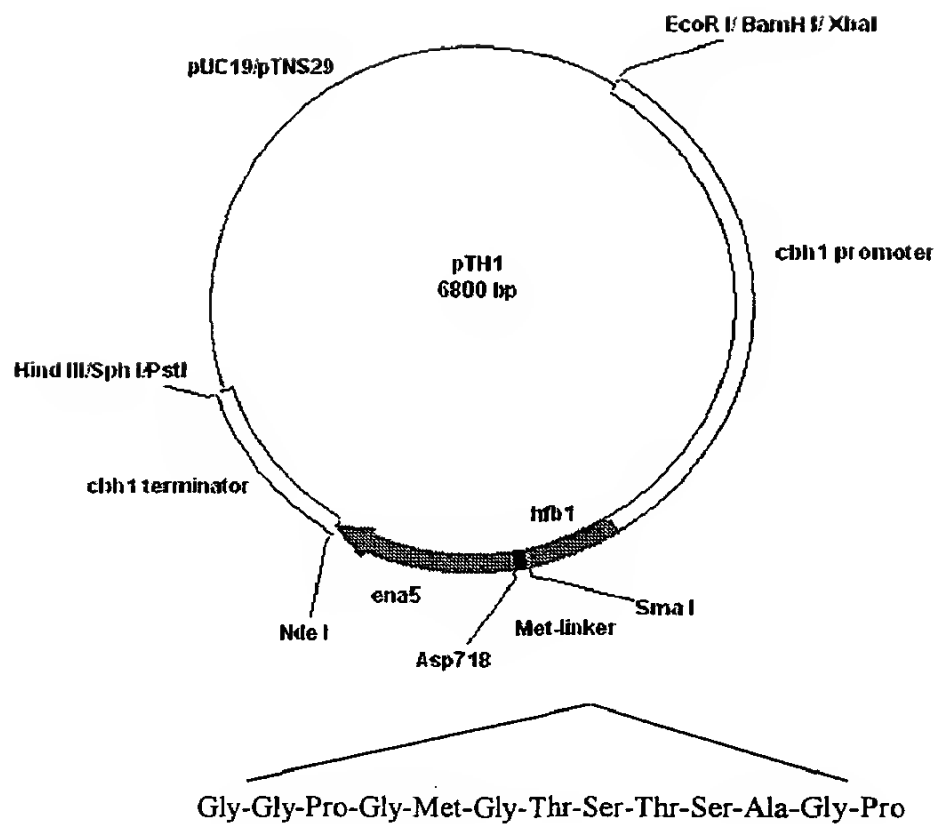


Figure 21

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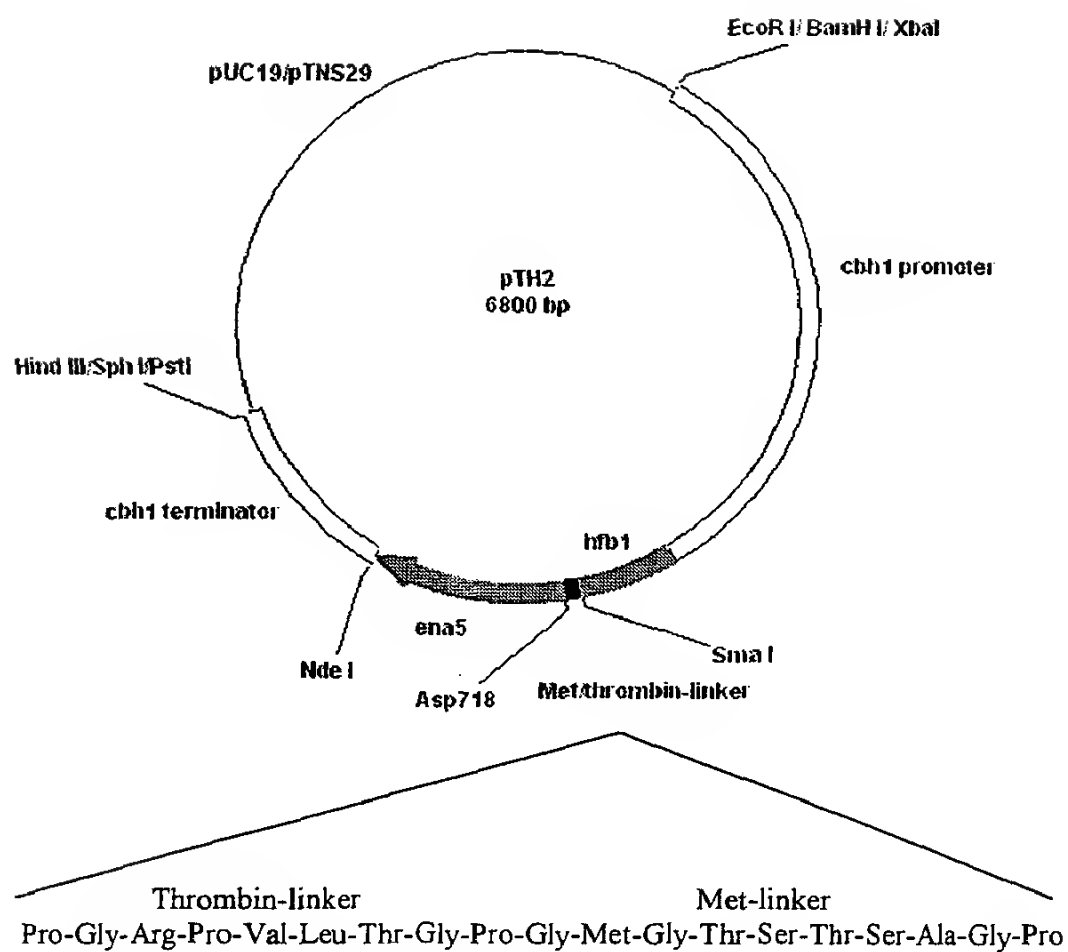


Figure 22

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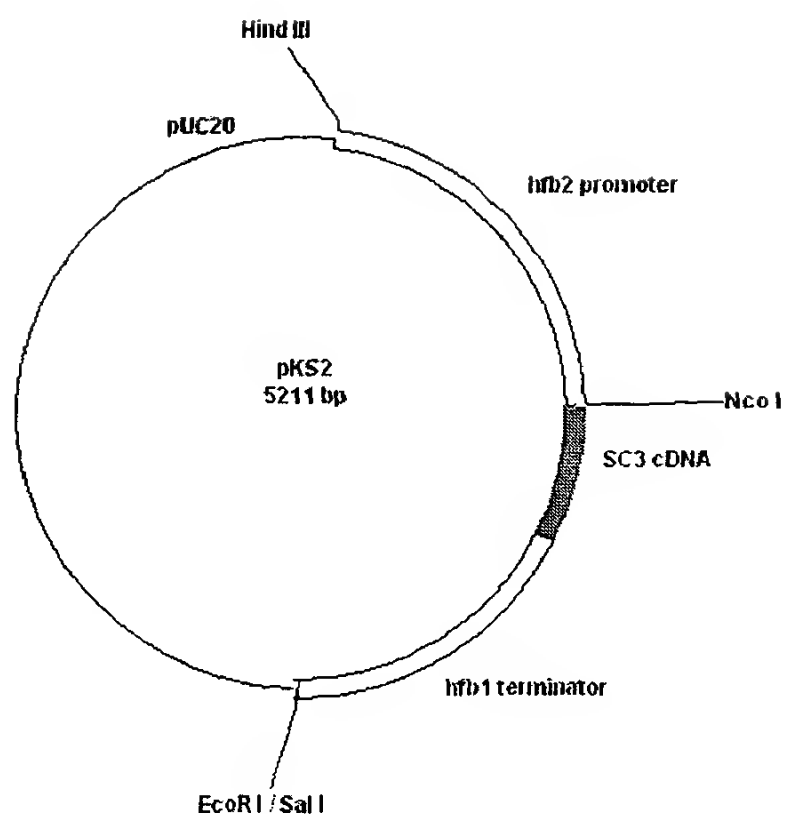
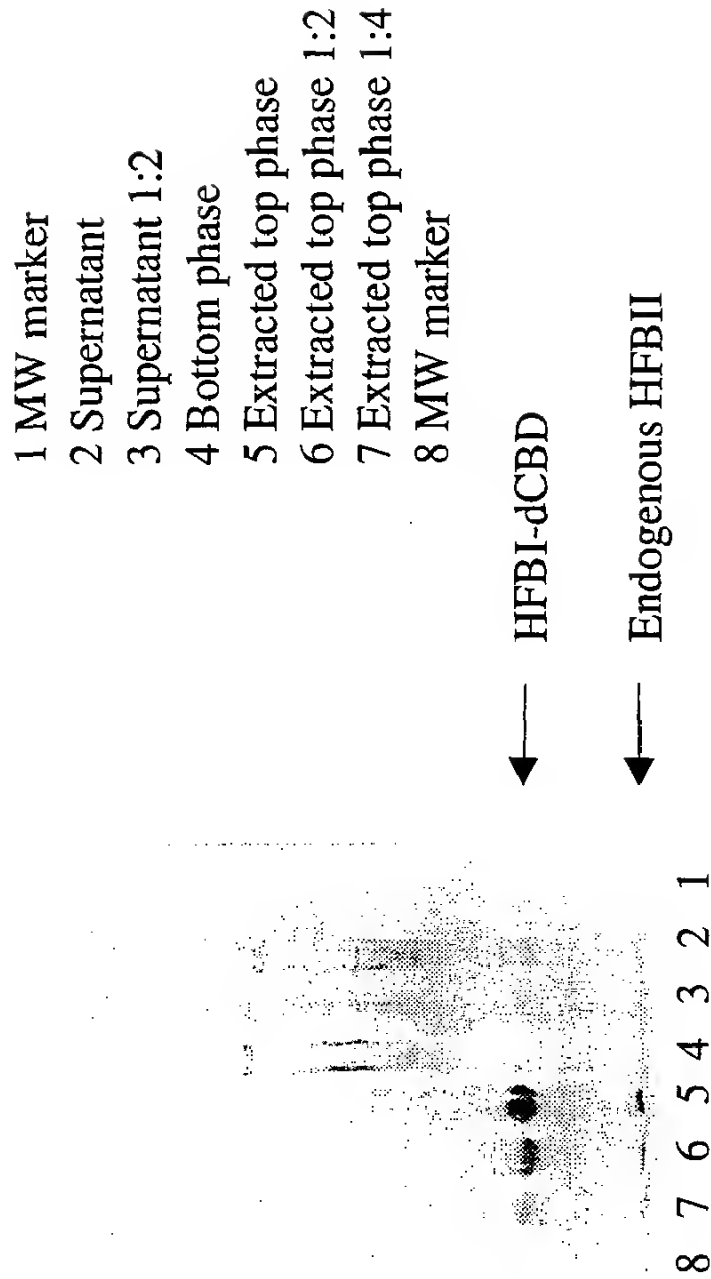


Figure 23

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Figure 24



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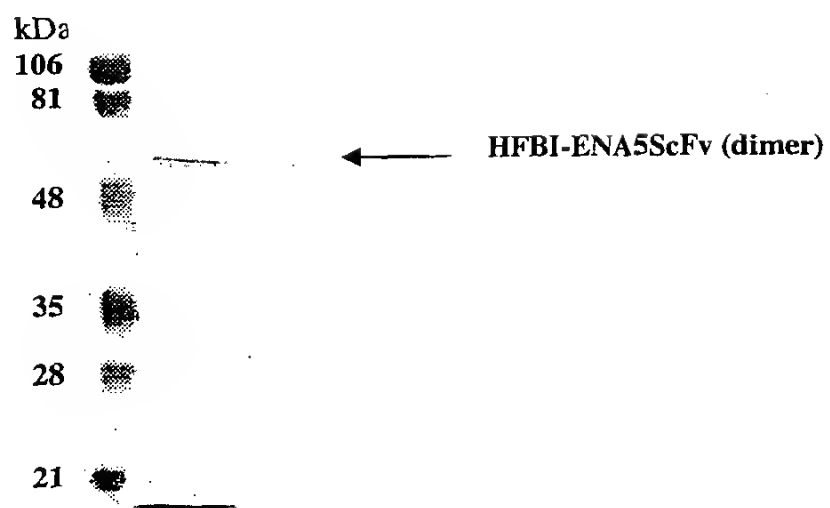


Fig. 25

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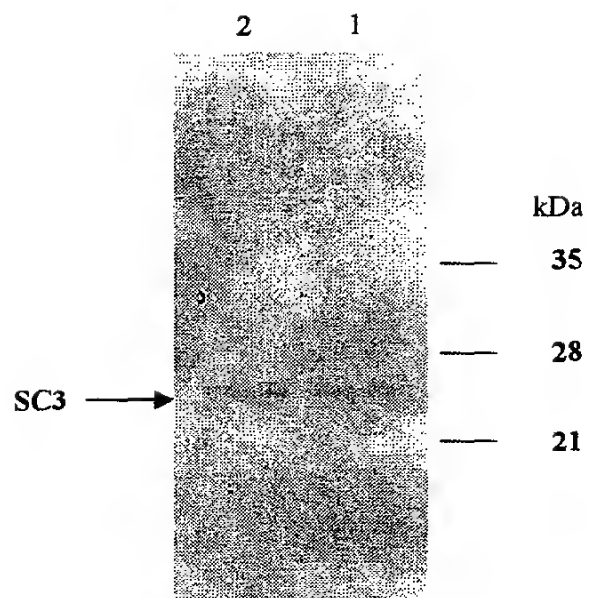


Fig. 26

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HFBI 2% Berol 532

K > 1000

vol. factor = 22,6

yield (teor) = 98%

yield (pract) = 80%

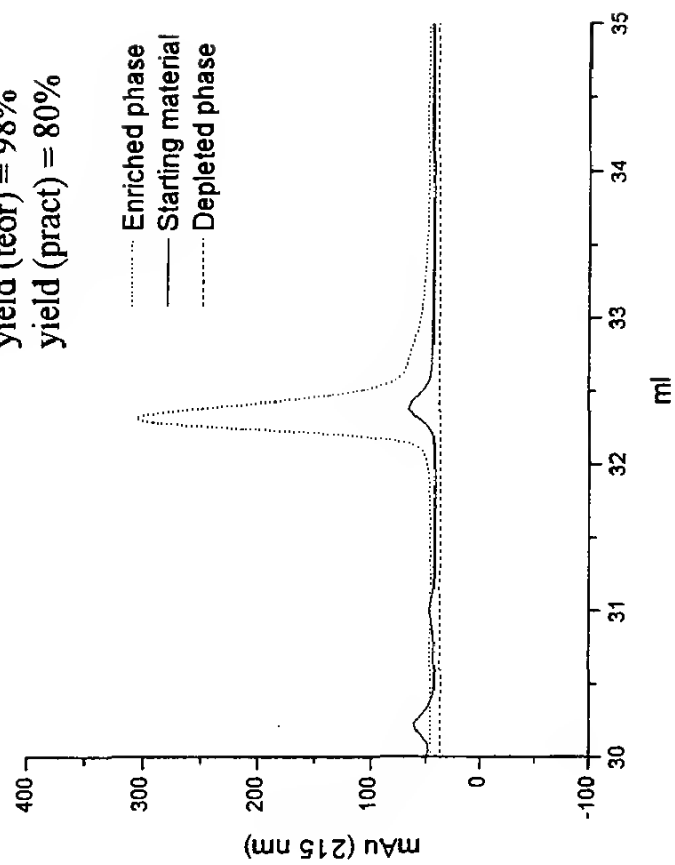


Figure 27

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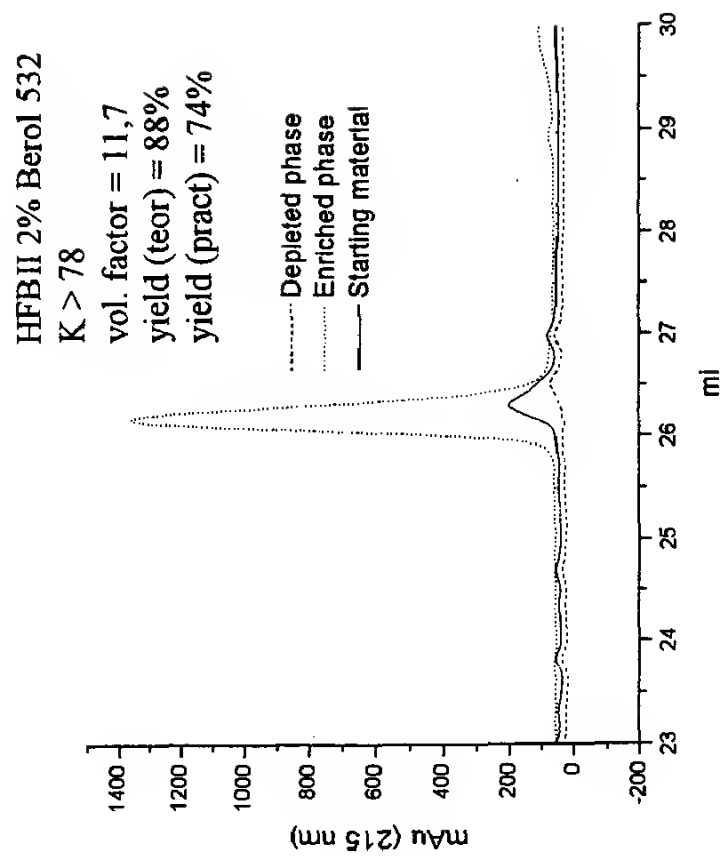


Figure 28

SEQUENCE LISTING

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tctctgctgc gtggcccccg ttgtaagttg atgccccagc tcaagctcca gtctttggca 360
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<211> 78

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<213> Artificial Sequence

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tctagttctg gaaccgca                                         78
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 <211> 30
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 <213> Artificial Sequence

<220>
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<210> 4
 <211> 63
 <212> DNA
 <213> Artificial Sequence

<220>
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 ggc 63

<210> 5
 <211> 2211
 <212> DNA
 <213> *Trichoderma reesei*

<220>
 <221> promoter
 <222> (1) .. (2211)
 <223> *cbh1* promoter sequence

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 tagattgggg agaagttgac ttccgcccag agctgaagg cgcacaaccg catgatata 180
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<211> 1588

<212> DNA

<213> *Trichoderma reesei*

<220>

<223> *T. reesei* eg11 cDNA

<400> 6

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 <213> *Trichoderma reesei*

 <220>
 <221> terminator
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 <223> *T. reesei cbh1* terminator

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 <212> DNA
 <213> Artificial Sequence

<220>
 <223> Description of Artificial Sequence: annealed primer

<400> 8
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<210> 9
 <211> 16
 <212> DNA
 <213> Artificial Sequence

<220>
 <223> Description of Artificial Sequence: annealed primer

<400> 9
 ctagaccgcg gttaat 16

<210> 10
 <211> 1232
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 <213> *Trichoderma reesei*

<220>
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<223> *T. reesei* *gpd1* promotor

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<211> 1129

<212> DNA

<213> *Trichoderma reesei*

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<221> terminator

<222> (1)..(1129)

<223> *T. reesei* *gpd1* terminator

<400> 11

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<211> 5733
<212> DNA
<213> *Aspergillus nidulans*

<220>
<223> (1-5733) Sequence of plasmid pAN52-1

<220>
<221> promoter
<222> (1)..(2129)
<223> *A. nidulans* *gpdA* promoter

<220>
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<222> (2130)..(2304)
<223> *A. nidulans* *gpdA* gene

<220>
<221> terminator
<222> (2305)..(3071)
<223> *A. nidulans* *trpC* terminator

<220>
<221> misc_feature
<222> (3072)..(5726)
<223> pUC18 from SalI to EcoRI

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<213> Artificial Sequence

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<223> Description of Artificial Sequence: PCR 5' primer

<400> 13

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<210> 14

<211> 66

<212> DNA

<213> Artificial Sequence

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<223> Description of Artificial Sequence: PCR 5' primer

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<210> 15

<211> 30

<212> DNA

<213> Artificial Sequence

<220>

<223> Description of Artificial Sequence: PCR 3' primer

<400> 15

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<210> 16

<211> 33

<212> DNA

<213> Artificial Sequence

<220>

<223> Description of Artificial Sequence: PCR 5' primer

<400> 16

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<210> 17

<211> 37

<212> DNA

<213> Artificial Sequence

<220>

<223> Description of Artificial Sequence: PCR 3' primer

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<223> *S. cerevisiae* FL01 coding sequence

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<223> (609-857) *S. cerevisiae* CYC1 transcription terminator

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<223> *S. cerevisiae* URA3 gene

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<223> Description of Artificial Sequence: PCR 5' primer

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<220>
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<400> 26
ggaattccgc ggactgcgca tcatgaagtt cttcgccatc gcc 43

<210> 27
<211> 80
<212> DNA
<213> Artificial Sequence

<220>
<223> Description of Artificial Sequence: PCR 3' primer

<400> 27
tgaattccat atgttaggta ccaccggggc ccatgccggt agaagtagaa gccccgggag 60
caccgacggc ggtctggcac 80

<210> 28
<211> 31
<212> DNA
<213> Artificial Sequence

<220>
<223> Description of Artificial Sequence: PCR 5' primer

<400> 28
tgaattcggg acccaggctt gctcaagcgt c 31

<210> 29
<211> 34
<212> DNA
<213> Artificial Sequence

<220>
<223> Description of Artificial Sequence: PCR 3' primer

<400> 29

tgaattccat atgtcacagg cactgagagt agta

34

<210> 30

<211> 48

<212> DNA

<213> Artificial Sequence

<220>

<223> Description of Artificial Sequence: PCR 5' primer

<400> 30

gaattcggtta ccctcgctccc tcgcggtccc gccgaagtga acctggtg

48

<210> 31

<211> 34

<212> DNA

<213> Artificial Sequence

<220>

<223> Description of Artificial Sequence: PCR 3' primer

<400> 31

tgaattccat atgctaaccc cgtttcatct ccag

34

<210> 32

<211> 918

<212> DNA

<213> *Trichoderma reesei*

<220>

<221> terminator

<222> (1)..(918)

<223> *T. reesei hfb1* terminator

<400> 32

gatgcccgcc cggggtcaag gtgtgcccgt gagaaagccc acaaagtgtt gatgaggacc 60
 atttccggta ctgggaaagt tggctccacg tgtttgggca ggtttgggca agttgtgtag 120
 atattccatt cgtacgccat tcttattctc caatatttca gtacactttt cttcataaat 180
 caaaaagact gctattctct ttgtgacatg ccggaaggga acaattgctc ttggtctctg 240
 ttatttgcaa gtaggagtgg gagattcgcc ttagagaaag tagagaagct gtgcttgacc 300
 gtggtgtgac tcgacgagga tggactgaga gtgttaggat taggtcgaac gttgaagtgt 360
 atacaggatc gtctggcaac ccacggatcc tatgacttga tgcaatggtg aagatgaatg 420
 acagtgttaag aggaaaagga aatgtccgcc ttcagctgat atccacgcca atgatacagc 480
 gatatacctc caatatctgt gggaaacgaga catgacatat ttgtgggaac aacttcaaac 540
 agcgagccaa gacctcaata tgcacatcca aagccaaaca ttggcaagac gagagacagt 600
 cacattgtcg tcgaaagatg gcatcgtaac caaatcatca gctctcatta tcgcctaaac 660
 cacagattgt ttgccgtccc ccaactccaa aacgttacta caaaagacat gggcgaatgc 720
 aaagacctga aagcaaacc tttttgcgac tcaattccct cctttgtcct cggaatgatg 780
 atccttcacc aagtaaaaga aaaagaagat tgagataata catgaaaagc acaacggaaa 840
 cgaaagaacc aggaaaagaa taaatctatc acgcaccttg tccccacact aaaagcaaca 900
 ggggggggtaa aatgaaat 918

<210> 33
 <211> 26
 <212> DNA
 <213> Artificial Sequence

<220>

<223> Description of Artificial Sequence: PCR 5' primer

<400> 33
 gacctcgatg cccgcccggg gtcaag

26

<210> 34
 <211> 26
 <212> DNA
 <213> Artificial Sequence

<220>

<223> Description of Artificial Sequence: PCR 3' primer

<400> 34
 gtcgacattt cattttaccc ccctcg

26

<210> 35
 <211> 1190
 <212> DNA
 <213> *Trichoderma reesei*

<220>

<221> promoter

<222> (1) .. (1190)

<223> *T. reesei hfb2* promoter

<400> 35
 ctcgagcagc tgaagcttgc atgcctgcat cctttgtgag cgactgcata cattttgcac 60
 aactgcccgt cgacgtctct cttccgacct tggccagctg gacaagcaac acaccaatga 120
 cgctttgtat tattagagta tatgcaagtc tcaggactat cgactcaact ctacccaccg 180
 aggacgatcg cggcacgata cgccttcgtt ctcattggcc caagcagacc aactgcccct 240
 ggagcaagat tcagcccaag ggagatggac ggcagggcac gccaggcccc caccaccaag 300
 ccactccctt tggccaaatc agcttgcatg tcaagagaca tcgagctgtg ccttgaaatt 360
 actaacaacc agggatggga aacgaagcct gcttttggaa agacaacaat gagagagaga 420
 gagagagggg gagagacaat gagtgccaca aacctggtag tgctccgcca atgcgctctga 480
 aatgtcacat ccgagtcctg gggcctctgt gagaatgtcc agagtaatac gtgttttgcg 540
 aatagtcctc tttcttgagg actggatacc tacgataccc tttttgagtt gatgcggtgc 600
 tttcgaagta ttatctggag gatagaagac gtctaggtaa ctacacaaaa ggcctatact 660
 ttggggagta gcccaacgaa aggttaactc tacggcctct tagagccgtc atagatccta 720
 cagcctcttg gagccgtcat agatcacatc tgtgtagacc gacattctat gaataatcat 780
 ctcacatgag ccacatacta ctacatacgt gtctctgcct acctgacatg tagcagtggc 840
 caagacacca aggccccagc atcaagcctc cctacctatc ccttcattg tacagcggca 900
 gagagattgc gatgagccct ctccctacct acagacggct gacaatgtcc gtataccacc 960
 agccaacgtg atgaaaacaa ggacatgagg aacagcctgc gagagctgga agatgaagag 1020
 ggccagaaaa aaaagtataa agaagacctc gattcccgcc atccaacaat cttttccatc 1080
 ctcacagca cactcatcta caaccatcac cacattcact caactcctct ttctcaactc 1140
 tccaaacaca aacattcttt gttgaatacc aaccatcacc acctttcaag 1190

<210> 36
<211> 20
<212> DNA
<213> Artificial Sequence

<220>

<223> Description of Artificial Sequence: PCR 5' primer

<400> 36
aagcttgcat gcctgcatcc

20

<210> 37
<211> 26
<212> DNA
<213> Artificial Sequence

<220>

<223> Description of Artificial Sequence: PCR 3' primer

<400> 37
ccatggtgaa aggtggtgat ggttgg

26

<210> 38
<211> 13
<212> PRT
<213> *Trichoderma reesei*

<220>

<223> wild type *T. reesei* EGI peptide linker

<400> 38
Val Pro Arg Gly Ser Ser Ser Gly Thr Ala Pro Gly Gly
1 5 10

<210> 39
<211> 10
<212> PRT
<213> Artificial Sequence

<220>

<223> Description of Artificial Sequence: modified CBHII linker

<400> 39
Gly Ser Ser Ser Gly Thr Ala Pro Gly Gly
1 5 10

<210> 40
<211> 19
<212> PRT
<213> Artificial Sequence

<220>

<223> Description of Artificial Sequence: Met/Thrombin
linker

<400> 40

Pro Gly Arg Pro Val Leu Thr Gly Pro Gly Met Gly Thr Ser Thr Ser
1 5 10 15

Ala Gly Pro

<210> 41

<211> 13

<212> PRT

<213> Artificial Sequence

<220>

<223> Description of Artificial Sequence: Met-containing linker

<400> 41

Pro Gly Ala Ser Thr Ser Thr Gly Met Gly Pro Gly Gly
1 5 10

<210> 42

<211> 14

<212> PRT

<213> Artificial Sequence

<220>

<223> Description of Artificial Sequence: linker containing the thrombin
cleavage site

<400> 42

Gly Thr Leu Val Pro Arg Gly Pro Ala Gly Val Asn Leu Val
1 5 10

INTERNATIONAL SEARCH REPORT

International application No.

PCT/FI 00/00249

A. CLASSIFICATION OF SUBJECT MATTER

IPC7: C07K 1/14, C07K 19/00, C12N 15/62, C12N 1/15 // C12R 1:885
According to International Patent Classification (IPC) or to both national classification and IPC

B. FIELDS SEARCHED

Minimum documentation searched (classification system followed by classification symbols)

IPC7: C07K

Documentation searched other than minimum documentation to the extent that such documents are included in the fields searched

SE,DK,FI,NO classes as above

Electronic data base consulted during the international search (name of data base and, where practicable, search terms used)

C. DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
P,X	Journal of Chromatography A, Volume 839, 1999, Märten Svensson et al, "Aqueous two-phase systems containing self-associating block copolymers. Partitioning of hydrophilic and hydrophobic biomolecules", page 71 - page 83, see abstract --	1,5-9,20-24
X	Journal of Chromatography A, 1996, Mats Carlsson et al: "Effects of fused tryptophan rich peptides to a recombinant protein A domain on the partitioning in polyethylene glycol-dextran and Ucon-dextran aqueous two-phase systems", page 107 - page 117, see abstract and sections 1 and 2 --	1,5-9,20-24

☒ Further documents are listed in the continuation of Box C.☒ See patent family annex.

* Special categories of cited documents:

"A" document defining the general state of the art which is not considered to be of particular relevance

"E" earlier document but published on or after the international filing date

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"O" document referring to an oral disclosure, use, exhibition or other means

"P" document published prior to the international filing date but later than the priority date claimed

"T" later document published after the international filing date or priority date and not in conflict with the application but cited to understand the principle or theory underlying the invention

"X" document of particular relevance: the claimed invention cannot be considered novel or cannot be considered to involve an inventive step when the document is taken alone

"Y" document of particular relevance: the claimed invention cannot be considered to involve an inventive step when the document is combined with one or more other such documents, such combination being obvious to a person skilled in the art

"&" document member of the same patent family

Date of the actual completion of the international search

14 July 2000

Date of mailing of the international search report

20-07-2000

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INTERNATIONAL SEARCH REPORT

International application No.

PCT/FI 00/00249

C (Continuation). DOCUMENTS CONSIDERED TO BE RELEVANT

Category*	Citation of document, with indication, where appropriate, of the relevant passages	Relevant to claim No.
X	WO 9207868 A1 (KABI PHARMACIA AB), 14 May 1992 (14.05.92), see description, example 1 and claim 1 --	1,5-9,20-24
X	WO 9418330 A1 (UNILEVER PLC), 18 August 1994 (18.08.94) --	1,5-9,20-24
A	WO 9404673 A1 (OY ALKO AB), 3 March 1994 (03.03.94) --	16-18
A	Eur J Biochem, Volume 248, No 2, Sept 1997, Nakari-Setälä T et al, "Differential expression of the vegetative and spore-bound hydrophobins of Trichoderma reesei--cloning and characterization of the hfb2 gene", page 415 - page 423, see abstract --	16-18
A	Eur J Biochem, Volume 235, No 1-2, January 1996, Nakari-Setälä T et al, "Genetic and biochemical characterization of the Trichoderma reesei hydrophobin HFBI", page 248 - page 255, see abstract -- -----	16-18

INTERNATIONAL SEARCH REPORT
Information on patent family members

02/12/99

International application No.

PCT/FI 00/00249

Patent document cited in search report			Publication date	Patent family member(s)		Publication date
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WO	9418330	A1	18/08/94	AU	6139794 A	29/08/94
				EP	0682710 A	22/11/95
				FI	953792 A	10/08/95
				ZA	9400916 A	10/08/95
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WO	9404673	A1	03/03/94	AU	4712193 A	15/03/94
				CA	2142602 A	03/03/94
				EP	0656943 A	14/06/95
				FI	950779 A	13/04/95
				JP	8500733 T	30/01/96
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